



CT&F - Ciencia, Tecnología y Futuro

ISSN: 0122-5383

Instituto Colombiano del Petróleo (ICP) - ECOPETROL S.A.

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CT&F - Ciencia, Tecnología y Futuro, vol. 10, no. 2, 2020, pp. 17-26

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DOI: <https://doi.org/10.7440/res64.2018.03>

Available in: <https://www.redalyc.org/articulo.oa?id=46570665002>

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ARTICLE INFO

Received : August 07, 2020

Revised : September 02, 2020

Accepted : September 28, 2020

CT&F - Ciencia, Tecnología y Futuro Vol 10, Num 2 December 2020, pages 17 - 26

DOI : <https://doi.org/10.29047/01225383.269>



EFFECT OF IONIC STRENGTH IN LOW SALINITY WATER INJECTION PROCESSES

■ EFECTO DE LA FUERZA IÓNICA EN PROCESOS DE INYECCIÓN DE AGUA DE BAJA SALINIDAD

Gustavo-Adolfo, Maya-Toro^{a*}; Luisana, Cardona^b; Mayra, Rueda^b; Farid, Cortés^c

ABSTRACT

Low salinity water injection has been frequently studied as an enhanced oil recovery process (EOR), mainly due to promising experimental results and because operational needs are not very different from those of the conventional water injection. However, there is no agreement on the mechanisms involved in increasing the displacement of crude oil, except for the effects of wettability changes. Water injection is the oil recovery method mostly used, and considering the characteristics of Colombian oil fields, this study analyses the effect of modifying the ionic composition of the waters involved in the process, starting from the concept of ionic strength (IS) in sandstone type rocks.

The experimental plan for this research includes the evaluation of spontaneous imbibition (SI), contact angles, and displacement efficiencies in Berea core plugs. Interfacial tension and pH measurements were also carried out. The initial scenario consists in formation water (FW), with total concentration of 9,800 ppm (TDS) (IS ~ 0.17) and a 27 °API crude oil. Magnesium and Calcium brine were also used in a first approach to assess the effect of the divalent ions.

Displacement efficiency tests are performed using IS of 0.17, 0.08, and 0.05, as secondary and tertiary oil recovery and the recovery of oil increases in both scenarios. Spontaneous imbibition curves and contact angle measurements show variations as a function of the ionic strength, validating the displacement efficiencies. Interfacial tension and pH collected data evidence that fluid/fluid interactions occur due to ionic strength modifications. However, as per the conditions of this research, fluid/fluid mechanisms are not as determining as fluid/rock

RESUMEN

La inyección de agua de baja salinidad ha sido frecuentemente estudiada como un proceso de recobro mejorado (EOR), principalmente debido a resultados experimentales prometedores y dado que las necesidades operacionales no son muy diferentes a las de la inyección de agua convencional. Sin embargo, no existe consenso en los mecanismos por los cuales mejora el desplazamiento de aceite, solo en que está relacionado con un efecto en la humectabilidad. La inyección de agua es el método de recobro más utilizado y, considerando las características de los campos Colombianos, este estudio analiza el efecto de modificar la composición iónica de las aguas involucradas en dicho proceso; partiendo del concepto de fuerza iónica (FI) y para rocas tipo areniscas.

El diseño experimental para esta investigación incluye la evaluación de imbibiciones espontáneas (IS), ángulos de contacto y eficiencias de desplazamiento en rocas tipo Berea. También se considera la variación de la tensión interfacial y el pH. El sistema inicial se construyó con agua de formación con concentración total de 9,800 ppm (TDS) (FI ~ 0.17) y crudo de 27 °API. Salmueras de cloruro de Calcio y Magnesio también fueron utilizadas para evaluar el efecto de los iones divalentes.

Pruebas de eficiencia de desplazamiento fueron realizadas con agua de fuerza iónica de 0.17, 0.08 y 0.05, en escenarios de recobro secundario y terciario, presentando aumento de la recuperación de aceite en ambos casos. Las mediciones de imbibición espontánea y de ángulos de contacto presentaron variación con la fuerza iónica, validando los resultados de eficiencia de desplazamiento.

Las mediciones de tensión interfacial y pH indican interacciones fluido-fluido debidas al cambio en la fuerza iónica, sin embargo; para las condiciones de esta investigación, los mecanismos fluido-fluido no parecen tan determinantes como los fluido-roca.

KEYWORDS / PALABRAS CLAVE

Low salinity | Ionic strength | Wettability | Spontaneous imbibition | Contact angle | Core flooding.

Baja salinidad | Fuerza iónica | Humectabilidad | Imbibición espontánea | Ángulo de contacto | Eficiencia de desplazamiento.

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1. INTRODUCTION

Water injection with modified salinity is an emerging EOR technique where the chemistry of the water/brine/rock system plays a fundamental role in oil recovery. Due to the complex nature of these interaction, different mechanisms have been proposed to explain how the low salinity water injection can improve oil displacement [1],[2],[3],[4].

Rock wettability changes represent the main mechanism proposed to explain the effects of low salinity water injection. Different authors indicate that a modified (low) salinity generates alteration of this property, releasing oil drops stuck to the rock surface (clay minerals). Alexander Rock [5] concludes that wettability alteration is the most relevant recovery mechanism, followed by fine migration, while multi-component ion exchange double-layer expansion is less crucial. Ligthelm [6], in experimental research for sandstones, suggests that a reduction in the ionic strength of the brines generates a multi cation exchange that alters wettability and increases displacement efficiency. Vledder [7] shows, at reservoir scale, that low salinity water injection produces a wettability change and a higher oil recovery. Berg [8] provided experimental evidence that the emulsion generation, fines migration, and decrease in interfacial tension are not relevant. Conversely, this study concluded that wettability alteration by double-layer expansion and cation exchange represents the dominant microscopic mechanism in low salinity water injection. Mamonov [9], argues that, although in the literature wettability is one of the most important mechanisms, it depends on the adsorption of compounds from the heavy fractions of crude oil. It is complex to establish the reservoir's wettability as it implies chemical interaction with rock minerals, formation water, and surfactant compounds from crude oil. Most of the mechanisms

proposed to explain the effects of low salinity water injection are based on the presence of clays, polar compounds in the oil, and divalent ions in the involved brines.

Wettability alteration of the reservoir rock due to the interactions with brine and/or oil is a critical variable that still needs further understanding of the proper development of modified water injection. Interaction between water and oil could also generate wettability changes as it can produce the release of oil or water content from the rock. At a pore-scale, wettability defines the trajectories of oil and brine, as well as the phase that covers the rock surface and the capillary pressure curves that determine the pore volume distribution of fluids [10]. Spontaneous imbibition tests are a well-known method to evaluate reservoir rock wettability [4]. However, its static character makes it necessary to consider some other measurements to quantify the wettability tendency and the recovered oil [1], where displacement tests in porous media are essential.

This research delves into whether modified salinity water is more effective than reservoir brine in the oil recovery of a Colombian field. Therefore, core flooding tests were carried out using formation water and the same water with different degrees of salinity dilution (ionic strength), measuring pressure profiles, effective oil permeabilities, and displacement efficiency. Spontaneous imbibition and contact angle tests were conducted to understand possible wettability changes. Interfacial tension and pH data were also gathered. Additionally, the same ionic strength is considered with equivalent brines of calcium and magnesium ions to evaluate their influence in the fluid:rock assessed systems.

2. EXPERIMENTAL DEVELOPMENT

FLUIDS CHARACTERIZATION

This study considers a 27 °API Colombian crude oil with 10.5 cP @ 60 °C. Oil properties are shown in **Table 1**. The basic number (BN) was not reported in this study; however, recent research has shown its importance in sandstones [9]. **Table 2** corresponds to the characterization of the formation brine (FB1) used for the tests, with an approximate concentration of total dissolved solids (TDS) of 9,800 ppm and IS of 0.17 (IS=0.17= 0.17 M NaCl). This brine is diluted in different proportions until reaching IS 0.08 (FB2) and IS 0.05 (FB3). Additionally, synthetic CaCl₂ and MgCl₂ brines were prepared in concentrations that allow having the IS of FB1 and FB2, respectively. All the brines were prepared using reactive grade Merck products.

Table 1. Physicochemical crude oil properties.

Viscosity 30 °C (cP)	37.3
Viscosity 60 °C (cP)	10.5
TAN (mgKOH/g)	0.21
API°	27
Saturated (%w)	41.94
Aromatic (%w)	30.85
Resins (%w)	22.72
Asphaltenes (%w)	4.49

Table 2. Physicochemical properties of the formation brine (FB1).

Ion	Formation water* Concentration (mg/L)
Na ⁺	2,954
K ⁺	91.65
Ca ⁺⁺	469
Mg ⁺⁺	62.03
Ba ⁺⁺	38.02
Sr ⁺⁺	28.27
HCO ₃ ⁻	1,403
SO ₄ ⁼	4
Cl ⁻	4,715
TDS	9,765
Ionic strength	0.17

*FB2 and FB3 are dilutions of this same brine in percentages of 50 and 70%, respectively.

ROCK CHARACTERIZATION

Berea rock samples were used for core flooding, spontaneous imbibition, and contact angle tests, using reservoir fluids of the

Table 3. Basic petrophysical properties of the porous media. Berea and crude supported sand.

ID	Length (cm)	Diameter (cm)	Pore volume (cm ³)	Porosity (%)	Klinkenberg permeability (mD)
B	5.84	3.70	13.6	21.7	306
Berea – Spontaneous imbibition & contact angles tests					
C	1	3.7	14.9	22.2	576
Crude supported sand – Spontaneous imbibition & contact angles tests					
IS 0.08					
D1*	1	3.7	1.42	12.5	NA
D2**	1	3.7	1.49	13.2	NA
D3***	1	3.7	1.46	12.9	NA
IS 0.17					
E1*	1	3.7	1.17	10.3	NA
E2**	1	3.7	1.44	12.7	NA

*MgCl₂ Brine / **CaCl₂ Brine / ***MgCl₂ + CaCl₂ Brine.

field being evaluated. Furthermore, spontaneous imbibition and contact angle tests were also carried out using crude oil supported unconsolidated Ottawa sand (0.8 g oil / 12 g sand), and reservoir fluids and Calcium and Magnesium synthetic brine. The details of the porous media are shown in Table 3.

The characterization of the Berea elemental and mineralogical composition was carried out using a QUANTA™ electronic microscope, coupled with an X-ray system using scattered energy (SEM-EDS). The results (Figure 1) show a quartz composition with frequent clear pores and some clay minerals like Kaolinite in loose sheets and grouped between the pores and Illite on the grains and at its edges.

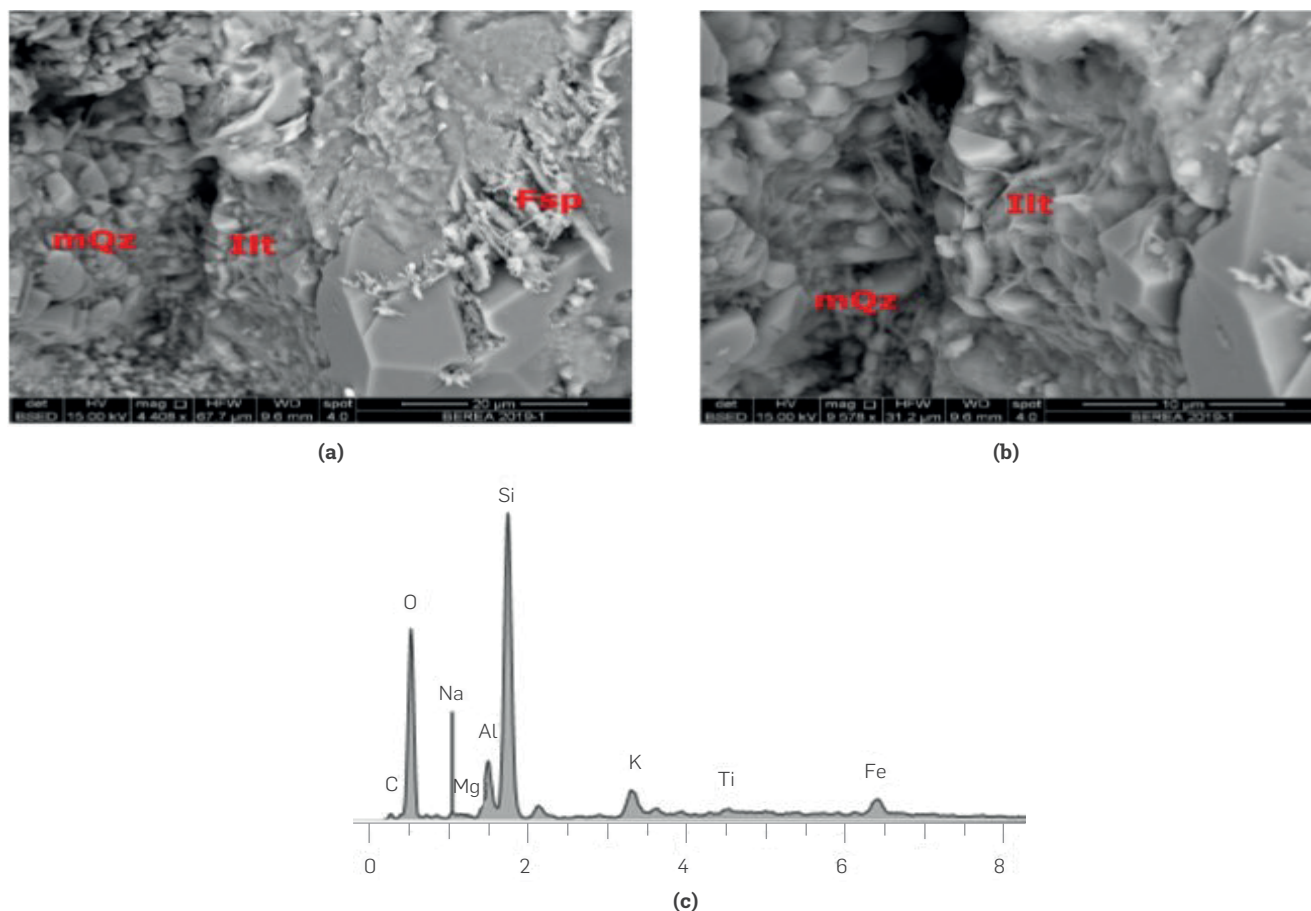


Figure 1. Images and elemental composition of the Berea. Quartz with some clay minerals (Kaolinite and Illite). Electron Microscopy Laboratory. Centro de Innovación y Tecnología, I.C.P.

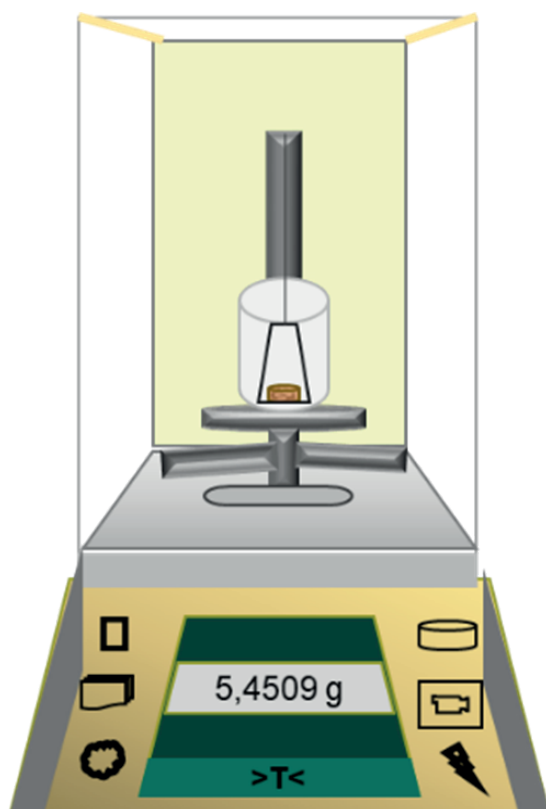


Figure 2. Analytical balance for the spontaneous imbibition tests.

METHODS

STATIC TESTS – SPONTANEOUS IMBIBITION, CONTACT ANGLES, INTERFACIAL TENSIONS

Spontaneous imbibition. To assess changes in the wettability of the mineral surfaces, the Berea sandstone, and the crude supported sand samples are contacted with the crude oil and the brines.

For the Berea case, the contact times of the fluids with the sample are the same as for the core flooding displacements. Three stages were carried out: (i) rock in formation brine FB1, FB2, and FB3; (ii) rock in crude oil; and (iii) rock in the same formation brine of stage (i). For the crude supported sand samples, three stages were also executed, which are described as follows, (i) the rock is in contact with brine FB1; (ii) rock in crude oil; and (iii) the rock samples are in contact with synthetic Ca^{2+} , Mg^{2+} or $\text{Ca}^{2+} + \text{Mg}^{2+}$ brine. The contact times are controlled using the behavior of the weight curve for every sample. All tests were performed at a temperature of 30°C.

Throughout the exposition times of the samples in the fluids, the change in weight is observed using an analytical balance (Figure 2). The data is reported in a time vs. sample weight change plot, where m_i is the initial weight in time i , and m_{i+1} is the gained weight in time $i+1$.

Contact angle. Contact angles are a quantitative measurement of wettability on the surface at a specific point. The results are obtained suspending a drop of the studied fluid at a representative point of the rock surface, and it is executed at the end of every spontaneous imbibition stage. The equipment used for this test is an optical tensiometer OCA 25 (OCA 25 PMC 750). In every angle measurement, two values are considered, right angle and left

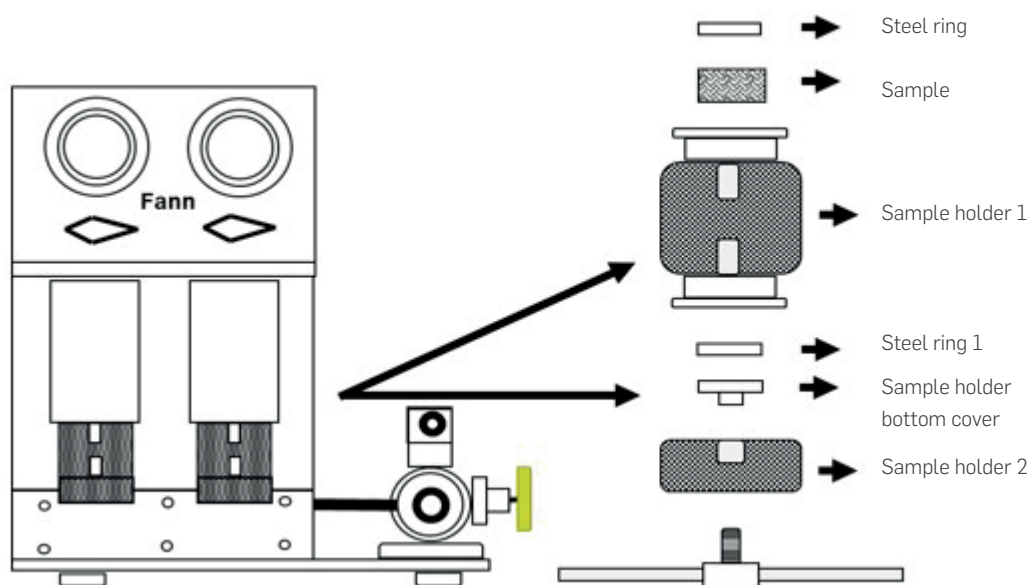


Figure 3. Fann compactor for preparing crude oil supported sand samples. Cements and drilling fluids laboratory. Centro de Innovación y Tecnología, I.C.P.

angle of the drop on the surface. The drop volume in this study is 15 μL . Once the drop is on the surface, a lens captures the image, which is processed in the equipment software. The forms obtained are analyzed considering the pendant drop and the sessile drop method. **Figure 3** is the schematic of the compactor equipment used to build the crude oil supported sand samples. **Figure 4** shows the representation of the optical tensiometer for contact angle measurements used in this study.

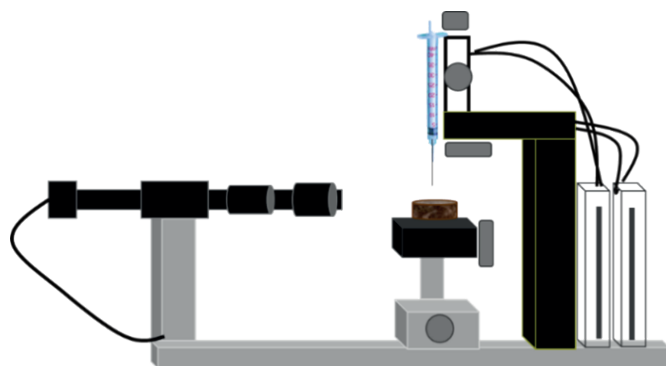


Figure 4. Representation of the optical tensiometer equipment (OCA 25 PMC 750) for contact angle measurement. Production chemistry laboratory. Centro de Innovación y Tecnología, I.C.P.

Interfacial tension. The interfacial tension between crude oil and brines was obtained using the Du Noüy ring method.

CORE FLOODING – SECONDARY AND TERTIARY OIL RECOVERY – DISPLACEMENT EFFICIENCIES

Displacement efficiency in porous media. The core flooding tests consisted of an oil recovery evaluation in secondary and tertiary

mode. In the first case, approximately six pore volumes (PV) of brine were injected to obtain the absolute permeability of the system. Then, the crude oil was injected to find the oil effective permeability to irreducible water saturation ($K_{oe} @ Sw_{ir}$). Once the pressure drop is stable, FB1 (IS = 0.17) is injected to run the displacement efficiency. When the oil production ends, and the pressure drop is steady again, the effective water permeability to residual oil saturation is obtained ($K_{we} @ Sor$). At this point, the system is resaturated with oil ($K_{oe} @ Sw_{ir}$) to perform the displacement efficiency with FB2 (IS = 0.08) and FB3 (IS = 0.05) brines, respectively.

For the tertiary oil recovery evaluation, FB1 (IS = 0.17) is injected until Sor ($Sor @ FB1$), then FB2 (IS = 0.08) is injected until a new Sor is reached ($Sor @ FB2$) and, finally, the injection of FB3 (IS = 0.05) is performed until no more oil is produced. **Figure 5** shows an outline of the core flooding equipment.

3. RESULTS

EFFECT OF THE IONIC STRENGTH CHANGE IN THE AQUEOUS PHASE

For analyzing the impact of the water injection ionic strength in modified salinity water injection processes, formation water (FB1) is injected with a total dissolved solids concentration (TDS) of 9,800 ppm and IS 0.17. The approach used to assess the effects of the IS was to dilute the initial brine of IS 0.17 (FB1) with distilled water to generate lower salinity brines FB2 (IS = 0.08) and FB3 (IS = 0.05), respectively.

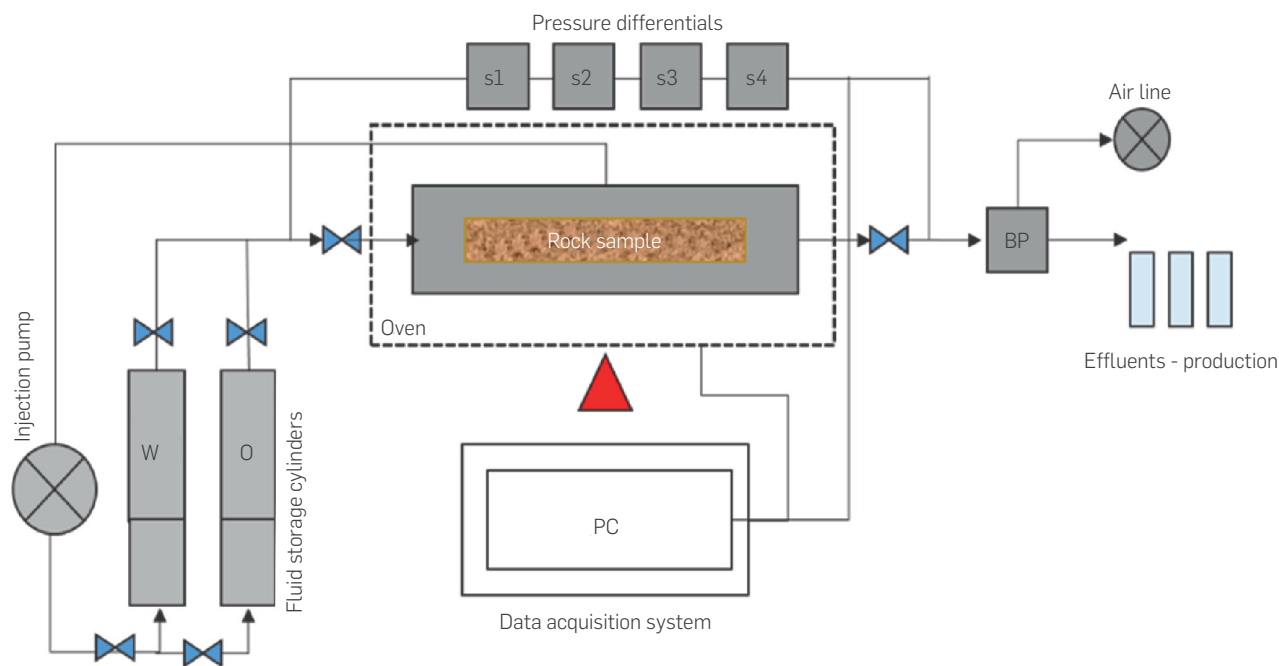


Figure 5. Core flooding equipment outline.

CORE FLOODING – SECONDARY AND TERTIARY OIL RECOVERY – DISPLACEMENT EFFICIENCIES

Table 4 shows the test conditions for the displacement efficiency measurements of water with different ionic strengths.

Table 4. Test conditions for the displacement efficiency measurements (IS 0.17 / 0.08 / 0.05).

Parameter	Value
Confining pressure (psi)	2,000
Pore pressure (psi)	200
Temperature (°C)	60
Rate (ml/min)	0.2
Brine viscosity @ 60 °C [cP]	0.48
Crude oil viscosity @ 60 °C [cP]	10.5

Formation water injection presents an absolute permeability of 135.5 mD, 55.7% less than the original Klinkenberg permeability. Next, crude oil is injected, obtaining an effective oil permeability (Koe @ Swir) of 86.23 mD. At this moment, the first displacement efficiency is developed using FB1. Once the system reaches residual oil saturation conditions (Sor @ FB1), FB2 is injected until reaching the new Sor (Sor @ FB2). At this point, the lower salinity brine (FB3) is injected until no more oil is produced. The oil production response is reported as a function of the injected pore volume (IPV) of each brine.

After injecting FB2 brine at So @ FB1, an additional 9% of oil is produced, which means that a reduction of approximately 50% in the ionic strength can increase oil mobility as a tertiary recovery method. However, a further decrease (From 0.08 to 0.05) of the ionic strength does not result in additional oil production (Figure 6). This behavior is possibly due to a charge redistribution at the mineral surface, preferring the low ionic strength water cations, and releasing oil drops attached by polar interaction [11],[12],[13]. The pressure drop observed is characteristic of coreflood water injection processes, stabilizing and reaching its lowest point when only one phase is flowing (FB3).

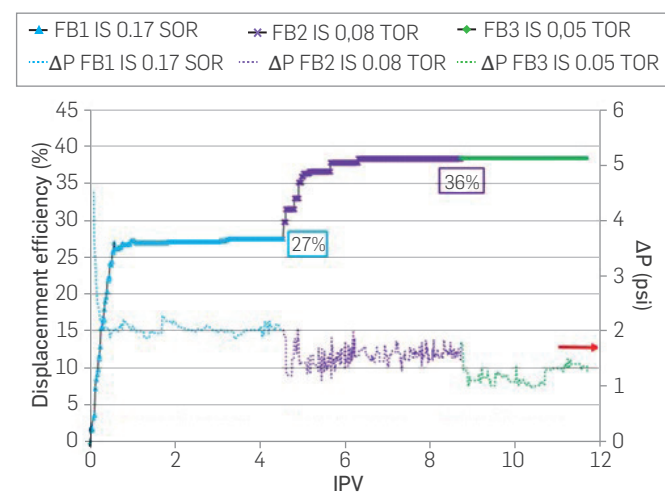


Figure 6. Displacement efficiency as tertiary oil recovery for FB1, FB2, and FB3 (rock samples B). (SOR) Secondary Oil recovery, (TOR) Tertiary Oil Recovery.

For assessing the displacement efficiency as a secondary recovery process with FB2 and FB3 brines, the sample is saturated with crude oil before each water injection, obtaining, for example, the effective oil permeabilities (Koe1, Koe2, and Koe3) for each of the waterfloods (Figure 7). The Koe values obtained indicate an increase in the flow capacity when a reduction in ionic strength occurs. The high residual water saturation values are attributed to changes in salinity (IS) considered in the experimental protocol. These results are also consistent with the spontaneous emulsification observed with the crude oil used in this study [14], as it will be briefly discussed later in this section.

When FB1 is injected as secondary oil recovery, a displacement efficiency of 27% is obtained (Figure 8). Next, crude oil is injected to saturate the system again until reaching similar Swir. It is worth mentioning that prior to this experiment, the porous media was at residual oil saturation with FB3 brine from the tertiary recovery evaluation. Then, the FB2 brine was injected, and the displacement efficiency improved by 9%. Finally, the core plug is resaturated with

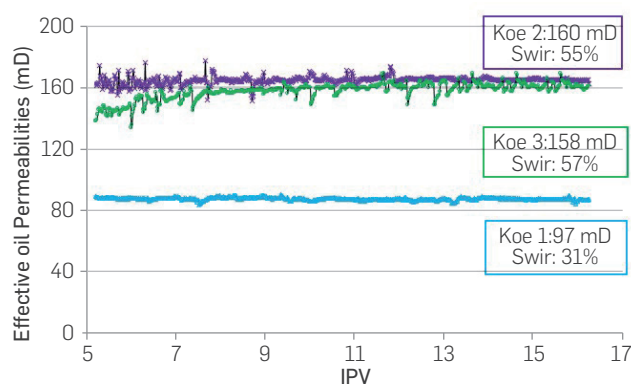


Figure 7. Effective oil permeabilities after injection of FB1, FB2, and FB3. Sample B in Table 3.

oil until reaching Swir to begin injecting FB3 brine (IS = 0.05). The displacement efficiency observed in this experiment was 24% and 15% higher than those recorded injecting FB1 (IS = 0.17) and FB2 (IS = 0.08), respectively (Figure 8). These results suggest that a decrease in salinity (IS) in the Berea coreflood using the crude oil under evaluation improves the displacement efficiencies regardless of the higher Swir at the beginning of the test injecting FB2 and FB3 (Figure 7). As already mentioned, the crude oil used in this study shows a natural tendency to form a microdispersion with decreased water salinity (IS) [14]. The latter can explain the increase in Swi observed when resaturating the Berea core plug with reservoir oil in the presence of high water saturation (Sorw) at lower IS. Although these experiments might not be comparable due to the effects of oil:water interactions, it is clear that oil can be recovered by decreasing water salinity. Hence, a new set of corefloods is underway considering a different oil resaturation approach. For example, the updated protocol considers the injection of FB1 brine after every experiment until no salinity changes are observed before the oil saturation stage. However, the results of these experiments are beyond the scope of this paper.

The effluents at the end of every secondary recovery stage were collected and maintained in a temperature control environment to measure pH (@25°C), as shown in Figure 9. In general, the changes in pH recorded during the three corefloods were relatively small (<0.6) and varied depending on the IS strategy. The most considerable pH change was obtained after flowing FB3, which is the experiment with the higher displacement efficiency observed at

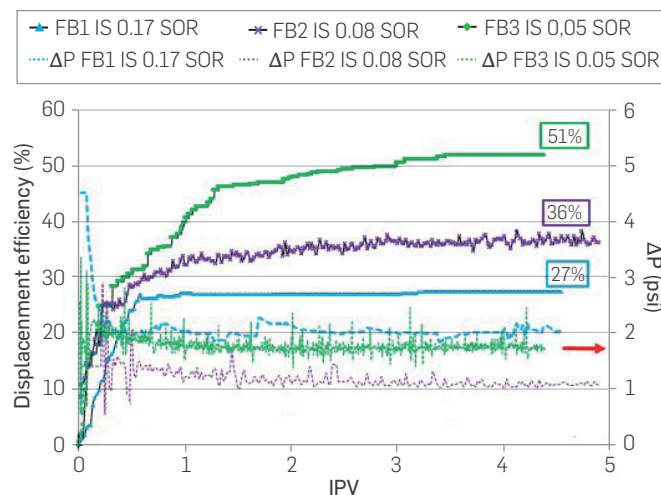


Figure 8. Displacement efficiency of real brine with different ionic strengths. Sample B in Table 3. Secondary oil recovery (SOR).

Swi (Figure 8). These results indicate that there is variation of pH with the different displacement efficiency stages. These results are consistent with different studies that show the relation between pH and low salinity effects [15]. However, the effect of changes in pH still requires further research.

The pH increase is attributed to the presence of clays in the rock, generating a possible cations exchange with the injected water [16] [17]. When brine with lower ionic strength is injected, the mineral surface may have exhausted its full capacity of ion exchange, with only free cations been exposed.

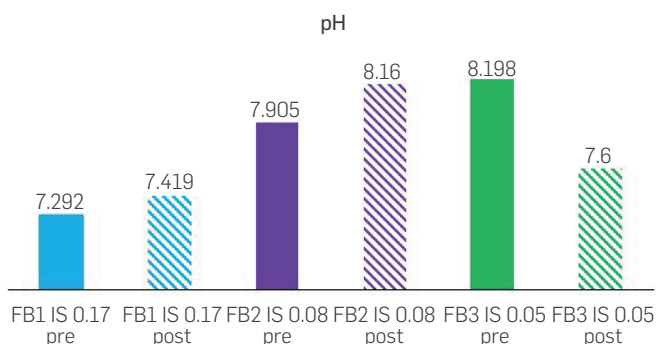


Figure 9. pH values (@25°C) before and after the injection of FB1, FB2, and FB3 brine.

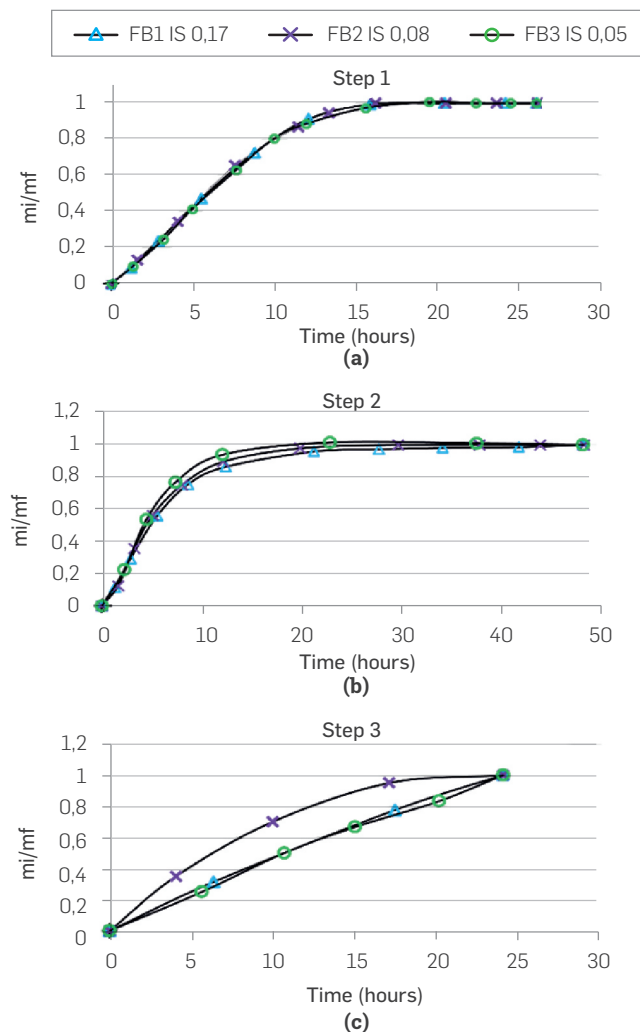
The crude oil used in this study has a low TAN (0.2). Although the generation of natural surfactants from residual oil (saponification) seems unlikely, the higher differential pressures and Swir observed with lower IS brines (FB2 and FB3) suggest some type of oil:water interactions. Hence, large variations in pH were not observed to justify it as a possible recovery mechanism [18]. The potential formation of natural surfactants can reduce the water-oil interfacial tension (IFT) and make the rock more water wet [19]. However, in these experiments, IFT changes were minor, as discussed later in this paper. Some authors, RezaeiDoust et al. [20], have reported successful core flooding tests using low salinity in low TAN oil. On the other hand, some authors have not found a relation between the pH of the effluents and the low salinity injection [21].

The data collected, for the conditions of this research, does not allow for establishing the pH as a dominant oil recovery mechanism.

IMBIBITION CURVES, CONTACT ANGLES, AND INTERFACIAL TENSION

According to the results of displacements, for the construction of spontaneous imbibition curves, two scenarios are established. The first one corresponds to consolidated rocks (sample C in Table 3), with the same fluids and contact times. The second scenario uses crude oil supported sand samples (D and E in Table 3), although analyzing the effect of divalent cations (Ca^{2+} and Mg^{2+}) separately in the brines with IS of 0.08 and 0.17. In the tertiary recovery mode, these values presented a more substantial influence (Figure 6).

Consolidated samples: Figure 10 presents the saturation curves for the different samples. In a period of 25 hours, the porous media gain weight in the same proportion, suggesting that for all the ionic strength tested, the saturation process has the same behavior (Figure 10a). Subsequently, the rocks get in contact with crude oil, and as the curves have normalized values, it is possible to compare the behavior as a function of time (Figure 10b). The rock that gains more weight in this stage is for the FB3 brine (IS 0.05), which suggests that when the initial system has lower IS, it is more oil-wet.



* m_i is the initial weight in time i , and m_{i+1} is the gained weight in time $i+1$ to f .

Figure 10. Spontaneous imbibition tests. IS 0.17, 0.08, and 0.05.

The porous media saturated with oil are put in contact again with the same brine (Figure 10c). The sample that gains more weight faster corresponds to the FB2 brine, with a dilution equivalent of 50% vs the original brine FB1. This behavior shows that this ionic strength, 0.08, will have the best oil displacement when the rock is at irreducible saturation of the same water. This result is consistent with the displacement efficiency observed during the tertiary mode coreflood shown in Figure 6.

The results described above are complemented with contact angle measurements before and after the contact with oil, using the captive drop method (Table 5). It can be noticed that the system that gains more weight (FB2) coincides with a more significant change in the contact angle, which means the less oil-wet tendency.

Table 5. Left and right contact angles (CA) by captive drop method for the different ionic strength brine before and after oil.

	Contact angles (captive drop)					
	FB1 IS 0.17		FB2 IS 0.08		FB3 IS 0.05	
	Right	Left	Right	Left	Right	Left
Before Oil	145.7°	145.5°	122.4°	122.3°	138.2°	138.0°
After Oil	142.3°	142.5°	154.5°	154.8°	133.1°	133.0°

Unconsolidated samples: For this evaluation, the study was divided into two groups based on the IS of the divalent cation chloride solutions (CaCl_2 and MgCl_2) and its mixtures. The first group of samples compares the effects of Ca^{2+} , Mg^{2+} and its combination for an IS of 0.08. The second set of samples was evaluated with Ca^{2+} and Mg^{2+} solutions at an IS of 0.17. For all the analyses presented, the samples are saturated with oil until reaching Swir with FB1 brine (IS = 0.17). The contact angle measurements are executed after the last contact.

Figure 11 presents the spontaneous imbibition curves of the brines with divalent ions at the IS of 0.08.

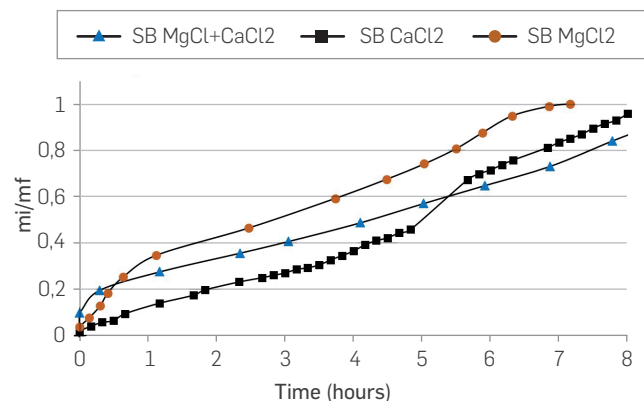


Figure 11. Spontaneous imbibition curves in unconsolidated porous media. Mg^{2+} , Ca^{2+} and $\text{Ca}^{2+} + \text{Mg}^{2+}$ synthetic brines at IS of 0.08.

MgCl_2 brine presents a higher affinity for the rock (Ottawa sand), followed by the CaCl_2 brine and the mixture of $\text{MgCl}_2 + \text{CaCl}_2$ at the same IS. As there is no clay in these samples, the result suggests that some components of the oil interact more with magnesium than with Calcium [16], and that fluid–fluid interaction can be strong, generating a multi-ion exchange between the oil, the formation

water, and the injection water. It is also possible that the Ottawa sand has some interaction directly with the fluids [22] [23].

On the other hand, Mg^{2+} and Ca^{2+} brine were evaluated with an ionic strength of 0.17. Figure 12 shows the spontaneous imbibition curves. In this last case (IS 0.17), the difference between divalent cations is not significant. However, during the first three hours, Mg^{2+} gains weight faster than Ca^{2+} . This trend changed during the last part of the test. The brines of Mg^{2+} and Ca^{2+} imbibes faster at an ionic strength of 0.17 than at 0.08. In both scenarios, the rock shows more preference for Mg^{2+} than for Ca^{2+} , which is more evident at IS 0.08.

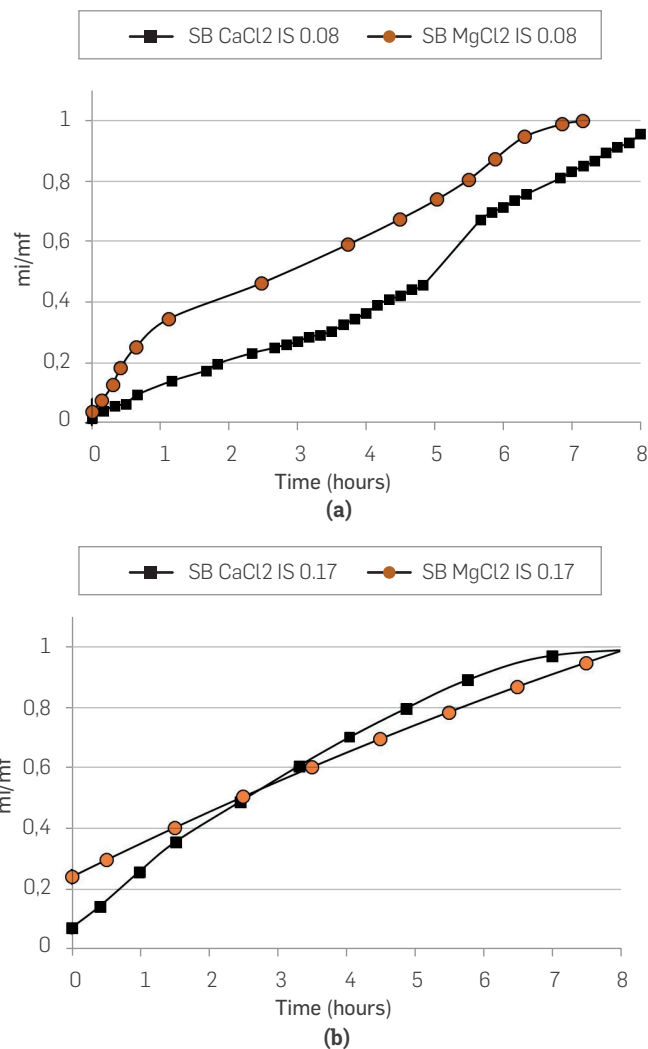


Figure 12. Parallel spontaneous imbibition curves in unconsolidated porous media. Synthetic Mg^{2+} and Ca^{2+} brine at an IS of 0.17 and 0.08.

The contact angle measurements in Table 6 corroborate the above mentioned results. The higher contact angle (IS 0.08) corresponds to MgCl_2 (131.6°), followed by CaCl_2 (124.6°) and $\text{MgCl}_2 + \text{CaCl}_2$ (108.1°). In Figure 12, the imbibition curves for IS 0.17 are quite similar, and the differences in the corresponding contact angles are considered within the experimental error.

Table 6. Contact angle values for crude supported sand / Brine IS 0.08 - 0.17 / crude oil.

Synthetic brine (IS 0.08)	Contact angle		Synthetic brine (IS 0.17)	Contact angle	
	Right	Left		Right	Left
MgCl ₂	131.6°	130.9°	MgCl ₂	145°	144.6°
CaCl ₂	124.6°	123.6°	CaCl ₂	148.2	147.1
MgCl ₂ +CaCl ₂	108.1°	108.6°			

Interfacial tensions: **Table 7** presents the interfacial tension between the crude oil and every brine considered in this study. The lowest IFT value in the case of consolidated samples occurred for FB2 (0.08), which indicates a mobility improvement of oil when decreasing ionic strength to 0.08. However, this behavior is not the same as for the tendency of produced oil (secondary case). It is possible that, for the conditions of this study, the mechanisms with more substantial influence are more related to fluid-rock than to fluid-fluid, or that the fluid-fluid mechanisms can not be identified using the interfacial tension.

Table 7. Interfacial tension values between crude oil and brines.

Oil phase	Aqueous phase	dyne/cm
Crude	FB1	27.61
Crude	FB2	23.80
Crude	FB3	25.15
Crude	SB MgCl ₂ IS: 0.08	28.37
Crude	SB CaCl ₂ IS: 0.08	28.21
Crude	SB CaCl ₂ + MgCl ₂ IS: 0.08	27.89

ACKNOWLEDGEMENTS

This work was undertaken as part of the agreement FP44842-338-2017 Doctorado Empresa, ECOPETROL – UNALMED - COLCIENCIAS. The data were kindly provided by Ecopetrol. The resources were provided by the National Fund for Financing Science, Technology and Innovation "Francisco Jose de Caldas".

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CONCLUSIONS

Displacement tests show the benefit of reducing the ionic strength of water as a tertiary recovery method. A decrease from 0.17 to 0.08 in IS provides an additional 9% oil recovery. A higher reduction, 0.08 to 0.05, does not allow improving the displacement efficiency suggesting that there is an optimal IS, or limited capacity in the reaction of the system, for this recovery process.

Given the protocol considered for the tests, it can be seen that, while the initial saturation water is of lower salinity than the injection water or vice versa, the ionic strength contrast between them produces improvements in the oil mobility. The foregoing opens up a range of possibilities for the use of this technology.

In Berea rock samples, applying both the spontaneous imbibition curves and the contact angles, FB2 brine (IS 0.08) generated a better displacement efficiency, which could imply that the reduction of the injection water's salinity must be carried to a limit to obtain the best behavior.

In unconsolidated samples, at IS of 0.17, magnesium brine displaced oil better in the early stage, but the final behavior was very similar to that of calcium brine. At IS of 0.08, the magnesium brine was more efficient in displacing the oil. These results highlight the importance of considering every ion independently, and not only the salinity reduction.

Given that the crude-oil supported samples did not contain clay, the differences in behavior observed suggest some water-oil interaction as an action mechanism for low salinity water injection.

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