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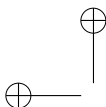
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Steady electrodiffusion in hydrogel-colloid composites: macroscale properties from microscale electrokinetics

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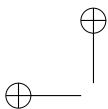
ABSTRACT

A rigorous microscale electrokinetic model for hydrogel-colloid composites is adopted to compute macroscale profiles of electrolyte concentration, electrostatic potential, and hydrostatic pressure across membranes that separate electrolytes with different concentrations. The membranes are uncharged polymeric hydrogels in which charged spherical colloidal particles are immobilized and randomly dispersed with a low solid volume fraction. Bulk membrane characteristics and performance are calculated from a continuum microscale electrokinetic model (Hill 2006b, c). The computations undertaken in this paper quantify the streaming and membrane potentials. For the membrane potential, increasing the volume fraction of negatively charged inclusions decreases the differential electrostatic potential across the membrane under conditions where there is zero convective flow and zero electrical current. With low electrolyte concentration and highly charged nanoparticles, the membrane potential is very sensitive to the particle volume fraction. Accordingly, the membrane potential – and changes brought about by the inclusion size, charge and concentration – could be a useful experimental diagnostic to complement more recent applications of the microscale electrokinetic model for electrical microrheology and electroacoustics (Hill and Ostoja-Starzewski 2008, Wang and Hill 2008).

Key words: electrodiffusion, electrokinetic phenomena, hydrogel-colloid composites, membrane potential, microhydrodynamics, soft composite materials, streaming potential.

INTRODUCTION

Hydrogels are an important class of soft matter that have gained widespread application in drug delivery (Qiu and Park 2001, Lin and Netters 2006, Peppas et al. 2000), tissue engineering (Khademhosseini et al. 2006, Langer 2007, Barndl et al. 2007, Drury and Mooney 2003), advanced materials (Peppas et al. 2000, Eddington and Beebe 2004, Chaterji et al. 2007), and molecular separations (Wang et al. 1993, Wang and Park 1998). Novel characteristics can be achieved by immobilizing organic and inorganic components



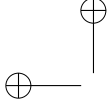
particulates in the polymer skeleton. For example, embedding gold or gold-coated silica nanoparticles into a thermally responsive hydrogel induces light-wavelength-sensitive swelling to achieve optically active microfluidic flow control (Sershen et al. 2005). In biosensing, immobilizing silica nanoparticles in polyacrylamide hydrogels and applying an electric field increase the otherwise diffusion-limited flux of uncharged macromolecules across the composite membrane (Matos et al. 2006). Other applications include delivering growth factors for bone regeneration (Chung et al. 2007), improving the contrast of ultrasound imaging for early tumor detection (Liu et al. 2006, Dayton and Ferrara 2002), and absorbing infrared energy for certain cancer treatment (Loo et al. 2005). Note also that polystyrene nanoparticles have been dispersed in neutral polyacrylamide hydrogels to increase the storage modulus and produce mechanoelectrical effects for artificial tactile perception and psycho-sensorial materials (Thévenot et al. 2007).

Hill (2006c, b) developed an electrokinetic transport model to quantify how imposed gradients of electrostatic potential, ion concentration, and pressure perturb an equilibrium state where each colloidal inclusion in the hydrogel-colloid composite is enveloped by a diffuse layer of counterions. Such an equilibrium is widely acknowledged to be reasonably well described by the non-linear Poisson-Boltzmann equation (Verwey and Overbeek 1948), which itself is a special case of a much more general electrokinetic transport (non-equilibrium) model (e.g., Overbeek 1943, Booth 1950). Similar methodologies have been adopted for ordered and random consolidated porous media with the immobile charge uniformly distributed on the solid matrix, often under conditions where the Debye length is smaller than the characteristic pore size (e.g., Gupta et al. 2007, Wang and Chen 2007).

Hill calculated perturbations to the equilibrium state of a single charged sphere immobilized in an uncharged porous medium (polymer hydrogel), and averaged the governing microscale equations to derive macroscale equations for dilute random dispersions, with transport coefficients derived from the microscale analysis of a single sphere. In principle, this theory could be advanced to handle higher particle concentrations by adopting cell models to account for particle interactions (e.g., Ahualli et al. 2006). Accordingly, the present macroscale equations are appropriate only when the inclusion volume fraction is sufficiently small, which, nevertheless, may often be the case. It should also be noted that the polymer skeleton is uncharged, so the immobile charge in the composite arises solely from the colloidal inclusions. Nevertheless, the calculations are valid for all practical values of the electrolyte concentration (Debye length), and particle size and surface charge density, which together determine the ζ -potential.

The hydrogel phase is modeled as a porous (Brinkman) medium with a very low volume fraction, so it hinders fluid flow due to hydrodynamic (Darcy) drag and viscous stresses, but does not hinder ion diffusion and electromigration. Predictions of the electroosmotic pumping capacity (termed the incremental pore mobility) and its relation to chemical and physical characteristics of the hydrogel and inclusions were recently found to compare well with experiments involving silica nanoparticles embedded in polyacrylamide (Hill 2007, Matos et al. 2006). Noteworthy is that the theoretical interpretation suggests that particle-particle and particle-polymer interactions (in the experiments) increase the effective hydrodynamic permeability of the hydrogel (Hill 2007).

The present model does not address elastic deformation, which is likely to be significant in situations



ELECTRODIFFUSION IN HYDROGEL-COLLOIDAL COMPOSITES

cally, electrically, and hydrodynamically) with the elastic polymer network (Hill 2006a, Hill and C Starzewski 2008, Wang and Hill 2008), thereby facilitating calculations of the particle displacement velocity when hydrogel-colloid composites are subjected to steady and oscillatory electric fields. experiments are relevant to the fields of microrheology (Cicuta and Donald 2007, Furst 2005, MacK and Schmidt 1999) and electroacoustics (Hunter 1998, O’Brien 1990, 1988), which are widely used to probe the microstructure of complex fluids, including colloidal dispersions, polymer solutions and g

This paper establishes a systematic methodology for calculating *macroscale* transport properties of hydrogel-colloid composites based on earlier *microscale* analysis in the literature (Hill 2006c, b). macroscale calculations are expected to complement experimental measurements of ion fluxes and membrane potentials. Accordingly, the paper begins by considering the continuum equations for an electrolyte in the absence of inclusions and hydrogel. This analysis of the well-known Poisson equation and ion-conservation equations is then used to rationalize an approximation (often referred to as the assumption) of bulk electroneutrality. The accompanying exact solution of this simple model provides a useful limiting case for interpreting subsequent numerical solutions of the non-linear coupled macroscopic equations for hydrogel-colloid composite membranes: namely Hill’s averaged ion-conservation equations and fluid mass and momentum conservation equations. Several striking aspects of the results are physically interpreted using previous knowledge of the underlying microscale electrokinetic phenomena.

ELECTRODIFFUSION IN THE ABSENCE OF POLYMER AND INCLUSIONS

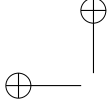
Here we consider electrodiffusion in an electrolyte without polymer or inclusions. Accordingly, the ions migrate by convection, diffusion and electromigration. If the fluid velocity is independently specified, the equations required to determine the electrostatic potential ψ and N ion concentrations n_j (z_j is the valence and D_j the diffusion coefficient with $j = 1 \dots N$) under steady conditions are the well-known Poisson and ion-conservation equations:

$$\begin{aligned} \nabla \cdot (\epsilon_o \epsilon_s \mathbf{E}) &= \sum_{j=1}^N n_j z_j e, \\ \nabla \cdot \mathbf{j}_j &= \nabla \cdot (-D_j \nabla n_j + z_j e \frac{D_j}{kT} n_j \mathbf{E} + n_j \mathbf{u}) = 0. \end{aligned}$$

If the average fluid velocity \mathbf{u} is specified, then this is a closed system of $N + 1$ equations involving ψ , $\mathbf{E} = -\nabla \psi$ and n_j as unknowns (ϵ_o is the vacuum permittivity, kT is the thermal energy, and e is the fundamental charge). Note that electrical neutrality is not imposed explicitly, since it should emerge naturally from the boundary conditions.

For a one-dimensional problem ($0 \leq x \leq L$) with uniform dielectric constant ϵ_s , the equations are

$$\epsilon_o \epsilon_s E_x = \sum_{j=1}^N n_j z_j e,$$



Note that the electrical current density is

$$i = \sum_{j=1}^N j_j e z_j, \quad (5)$$

so under conditions where $i = 0$ with a z - z electrolyte, $j_1 = j_2 = j$.

Alternatively, consider solving

$$-\epsilon_o \epsilon_s \psi_{xx} = \sum_{j=1}^N n_j z_j e, \quad (6)$$

$$-D_j n_{j,xx} - z_j e \frac{D_j}{kT} (n_{j,x} \psi_x + n_j \psi_{xx}) + n_{j,x} u = 0. \quad (7)$$

If the average fluid velocity u is specified, then a closed system of $N + 1$ equations must be solved with ψ and n_j as unknowns. However, while these equations could be solved with prescribed boundary conditions (at each end of the domain), the electrical current cannot be set to zero *a priori*. Rather, the electrostatic potential difference across the domain that yields zero electrical current must be established. Even so, a numerical solution may still be challenging because, as demonstrated below, the left-hand side of the Poisson equation above is extremely small compared to the right-hand side when the characteristic length scale is larger than the Debye length (typically between 1 and 100 nm).

ELECTRONEUTRALITY

Consider scaling the Poisson equation using a macroscopic length scale l_c , with electrostatic potential scale $\psi_c = kT/e$ and ion-concentration (charge density) scale n_c . Accordingly, the left-hand side is $O[(\kappa l_c)^{-2}]$ with respect to the right-hand side, with $\kappa^{-1} \sim [\epsilon_o \epsilon_s kT / (e^2 n_c)]^{1/2}$ the Debye length. Since κ^{-1} is of nanometer scale for charge densities in aqueous electrolytes, on macroscopic scales $(\kappa l_c)^{-2} \ll 1$. Therefore, in the ‘outer’ region where $l_c \gg \kappa^{-1}$ is indeed the appropriate length scale, the leading-order approximation of the Poisson equation becomes a statement of local electroneutrality, so the governing equations above become

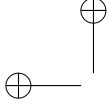
$$0 = \sum_{j=1}^N n_j z_j e, \quad (8)$$

$$-D_j n_{j,xx} - z_j e \frac{D_j}{kT} (n_{j,x} \psi_x + n_j \psi_{xx}) + n_{j,x} u = 0. \quad (9)$$

This important result was first established formally by MacGillivray (1968) using matched asymptotic expansions, and it is now widely adopted in standard texts. The following example establishes an explicit formula to be adopted in the following sections that address the much more difficult problem where charged colloidal inclusions are immobilized in an uncharged hydrogel skeleton.

For a z - z electrolyte, the bulk electroneutrality approximation requires $n_1 = n_2 = n$, so the ion-conservation equations are

$$D_1 \left(\frac{n}{l_c} \right) = 0 \quad (10)$$



or

$$\begin{aligned} j_1 &= -D_1 n_x + z_1 e \frac{D_1}{kT} n E + nu \\ j_2 &= -D_2 n_x + z_2 e \frac{D_2}{kT} n E + nu. \end{aligned}$$

Eliminating E gives

$$j_1/D_1 + j_2/D_2 = -2n_x + nu(1/D_1 + 1/D_2),$$

which is easily solved for $n(x)$ given a constant value of u .

When the current density $i = 0$, $j_1 = j_2 = j$ and

$$n(x) = n(0) + (j/u)[\exp(-\text{Pe}x/L) - 1],$$

so

$$j = \frac{u[n(L) - n(0)]}{[\exp(-\text{Pe}) - 1]}$$

with

$$\text{Pe} = uL/D^e \text{ and } D^e = 2/(1/D_1 + 1/D_2).$$

Note that with zero convective flux ($u = 0$),

$$j = -D^e n_x,$$

and

$$E(x) = -\psi_x = \frac{(\gamma - 1) kT n_x}{(1 + \gamma) n z_1 e} = \frac{(1 - \gamma) kT n_x}{(1 + \gamma) n z_2 e},$$

where $\gamma = D_1/D_2$ and $z_1 = -z_2$. Moreover, the potential difference across the membrane (membrane potential) is

$$\begin{aligned} \Delta\psi &\equiv -\int_0^L E(x) dx = -\frac{(\gamma - 1) kT}{(1 + \gamma) z_1 e} \int_0^L (n_x/n) dx \\ &= -\frac{(\gamma - 1) kT}{(1 + \gamma) z_1 e} \ln [n(L)/n(0)]. \end{aligned}$$

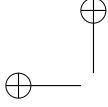
Let us examine the validity of the electroneutrality approximation by evaluating the left-hand side of the Poisson equation, which, recall, was neglected in reaching Eqn. (20):

$$\epsilon_o \epsilon_s E_x = -\frac{(\gamma - 1) \epsilon_o \epsilon_s kT}{(1 + \gamma) z_1 e} (n_x/n)^2.$$

This charge density is equivalent to a molar concentration of ions, each with charge $z_1 e$ (N_A is Avogadro's constant):

$$\frac{\epsilon_o \epsilon_s E_x}{10^3 N_A z_1 e} = -\frac{(\gamma - 1)}{(1 + \gamma)} \frac{\epsilon_o \epsilon_s kT}{10^3 N_A (z_1 e)^2} (n_x/n)^2.$$

It is easily verified that this concentration is generally extremely small unless the characteristic length scale is of the order of $O(\text{nm})$. For example, for KNO_3 , $\gamma = D_+/D_- \approx 73.5/71.46 \approx 1.029$. Therefore, with $n(0) = 1 \text{ mM}$



ELECTRODIFFUSION IN HYDROGEL-COLLOID COMPOSITE MEMBRANES

The averaged equations derived by Hill (2006b) are written below for unidirectional transport of a z - z electrolyte in hydrogel composites. Note that the electroneutrality approximation requires $\langle n_1 \rangle = \langle n_2 \rangle = \langle n \rangle$, and the fluid conservation (continuity) equation requires $\langle \mathbf{u} \rangle = \text{const.}$, so the remaining ion conservation equations and momentum equation are

$$\begin{aligned} \langle \mathbf{j}_j \rangle &= \langle n \rangle \langle \mathbf{u} \rangle - z_j e \frac{D_j}{kT} \langle n \rangle \langle \nabla \psi \rangle - D_j \langle \nabla n \rangle \\ &+ \phi(3/a^3) z_j e \frac{D_j}{kT} \langle n \rangle (-\langle \nabla \psi \rangle D^E + \langle \nabla n \rangle D^B + \langle \mathbf{u} \rangle D^U) \\ &+ \phi(3/a^3) D_j (-\langle \nabla \psi \rangle C_j^E + \langle \nabla n \rangle C_j^B + \langle \mathbf{u} \rangle C_j^U) \end{aligned} \quad (23)$$

and

$$\langle \nabla p \rangle = -(\eta/\ell^2) \langle \mathbf{u} \rangle - \phi(3/a^3)(\eta/\ell^2)(-\langle \nabla \psi \rangle C^E + \langle \nabla n \rangle C^B + \langle \mathbf{u} \rangle C^U). \quad (24)$$

These are more compactly written

$$\begin{pmatrix} \langle \mathbf{j}_1 \rangle \\ \langle \mathbf{j}_2 \rangle \\ \langle \nabla p \rangle \end{pmatrix} = \begin{pmatrix} A_{11} & A_{12} & A_{13} \\ A_{21} & A_{22} & A_{23} \\ A_{31} & A_{32} & A_{33} \end{pmatrix} \begin{pmatrix} \langle \nabla n \rangle \\ \langle \nabla \psi \rangle \\ \langle \mathbf{u} \rangle \end{pmatrix}, \quad (25)$$

where

$$A_{11} = -D_1 + \phi(3/a^3) z_1 e \frac{D_1}{kT} \langle n \rangle D^B + \phi(3/a^3) D_1 C_1^B \quad (26)$$

$$A_{12} = -z_1 e \frac{D_1}{kT} \langle n \rangle - \phi(3/a^3) z_1 e \frac{D_1}{kT} \langle n \rangle D^E - \phi(3/a^3) D_1 C_1^E \quad (27)$$

$$A_{13} = \langle n \rangle + \phi(3/a^3) z_1 e \frac{D_1}{kT} \langle n \rangle D^U + \phi(3/a^3) D_1 C_1^U \quad (28)$$

$$A_{21} = -D_2 + \phi(3/a^3) z_2 e \frac{D_2}{kT} \langle n \rangle D^B + \phi(3/a^3) D_2 C_1^B \quad (29)$$

$$A_{22} = -z_2 e \frac{D_2}{kT} \langle n \rangle - \phi(3/a^3) z_2 e \frac{D_2}{kT} \langle n \rangle D^E - \phi(3/a^3) D_2 C_2^E \quad (30)$$

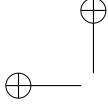
$$A_{23} = \langle n \rangle + \phi(3/a^3) z_2 e \frac{D_2}{kT} \langle n \rangle D^U + \phi(3/a^3) D_2 C_2^U \quad (31)$$

$$A_{31} = -\phi(3/a^3)(\eta/\ell^2) C^B \quad (32)$$

$$A_{32} = \phi(3/a^3)(\eta/\ell^2) C^E \quad (33)$$

$$A_{33} = -(\eta/\ell^2) - \phi(3/a^3)(\eta/\ell^2) C^U. \quad (34)$$

Note that the asymptotic coefficients: $D^E, C_1^E = C_2^E, C^E$; $D^B, C_1^B = C_2^B, C^B$; $D^U, C_1^U = C_2^U, C^U$ are, in general, functions of the local scaled particle radius κa , scaled ζ -potential $\zeta e/(kT)$, and scaled Brinkman screening length $\kappa \ell$ (or ℓ/a) for a given electrolyte [η is the fluid viscosity and ℓ^2 is the hydrodynamic (Darcy) permeability of the polymer skeleton]



provides an algebraic relationship between the two bulk ion fluxes. For the example below, however, is zero electrical current, so $\langle \mathbf{j}_1 \rangle = \langle \mathbf{j}_2 \rangle = \langle \mathbf{j} \rangle = \text{const}$.

It is helpful to write the macroscale equations above in a form that explicitly relates the unknown gradients of $\langle n \rangle$, $\langle \psi \rangle$ and $\langle p \rangle$ to the (co-linear) constants $\langle \mathbf{j}_1 \rangle$, $\langle \mathbf{j}_2 \rangle$ and $\langle \mathbf{u} \rangle$, *i.e.*,

$$\begin{pmatrix} \langle \mathbf{j}_1 \rangle \\ \langle \mathbf{j}_2 \rangle \\ \langle \mathbf{u} \rangle \end{pmatrix} = \begin{pmatrix} B_{11} & B_{12} & B_{13} \\ B_{21} & B_{22} & B_{23} \\ B_{31} & B_{32} & B_{33} \end{pmatrix} \begin{pmatrix} \langle \nabla n \rangle \\ \langle \nabla \psi \rangle \\ \langle \nabla p \rangle \end{pmatrix},$$

where

$$\begin{pmatrix} B_{11} & B_{12} & B_{13} \\ B_{21} & B_{22} & B_{23} \\ B_{31} & B_{32} & B_{33} \end{pmatrix} = \begin{pmatrix} A_{11} - A_{13}A_{31}/A_{33} & A_{12} - A_{13}A_{32}/A_{33} & A_{13}/A_{33} \\ A_{21} - A_{13}A_{31}/A_{33} & A_{22} - A_{13}A_{32}/A_{33} & A_{23}/A_{33} \\ -A_{31}/A_{33} & -A_{32}/A_{33} & 1/A_{33} \end{pmatrix}.$$

The components of matrix \mathbf{B} depend on $\langle n \rangle(x)$, so this non-linear system of equations must be solved for $\mathbf{y}(x) = [\langle n \rangle(x), \langle \psi \rangle(x), \langle p \rangle(x)]$, given a constant $\mathbf{b} = (\langle \mathbf{j}_1 \rangle, \langle \mathbf{j}_2 \rangle, \langle \mathbf{u} \rangle)$. This is easily achieved numerically integrating¹

$$\frac{d\mathbf{y}}{dx} = \mathbf{B}^{-1}[\langle n \rangle(x)]\mathbf{b}$$

with ‘initial condition’ $\mathbf{y}(x=0) = [\langle n \rangle(0), \langle \psi \rangle(0), \langle p \rangle(0)]$. Because $\mathbf{B}(x)$ is independent of $\langle \psi \rangle$ and $\langle p \rangle$, the solution provides $\Delta \mathbf{y} \equiv \mathbf{y}(x=L) - \mathbf{y}(x=0)$ in the parameter space comprising \mathbf{b} and $\mathbf{y}(x=0)$. In practical terms, this means the flux $j = |\langle \mathbf{j} \rangle|$, pressure differential $\Delta \langle p \rangle$, and electrostatic potential differential $\Delta \langle \psi \rangle$ can be calculated (implicitly) as a function of the bulk convective flow $u = |\langle \mathbf{u} \rangle|$, and the ion concentrations on each side of the composite membrane: *e.g.*, with $\Delta \langle n \rangle = \langle n \rangle(x=L) - \langle n \rangle(x=0)$ and $\langle n \rangle(x=0)$ as two independent scalars.

In general, such a computation is rather intensive, since, in addition to the bulk ion concentrations, the asymptotic coefficients vary with κa and $\zeta e/(kT)$ (with fixed ℓ/a), both of which are non-linear functions of $\langle n \rangle(x)$. However, the asymptotic coefficients can be computed beforehand, and subsequently interpolated from sufficiently refined tables. Representative values (and several other quantities derived from them) are provided in Tables I, II and III for NaCl electrolyte with $\ell/a = 0.1$ ($a = 10$ nm and $\ell = 1$ nm). For the macroscale computations presented below, the asymptotic coefficients were available for many more values of κa and $\zeta e/(kT)$. The reader is referred to Hill (2006a, c) for details of these microscale calculations and the physical significance of the other quantities provided². Note that it is straightforward to consider the inclusions to have a constant charge, in which case the ζ -potential varies with position according to the particle size and surface charge density, and the bulk electrolyte concentration (Verwey and Overbeek 1948, Russel et al. 1989).

The hydrogels for the calculations presented below have a Brinkman screening length $\ell = 1$ nm, which is representative of polyacrylamide (Hill 2007). The inclusion radius $a = 10$ nm, and the electrolyte (NaCl) is moderately asymmetric with $\gamma = D_1/D_2 \approx 1.33/2.33$. Note that the dimensionless parameter $\ell/a = 0.1$, whereas previous microscale calculations reported in the literature for NaCl have $\ell/a \approx 0.01$.

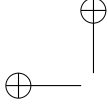
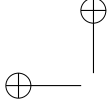


TABLE I

Scaled (dimensionless) asymptotic coefficients for bulk *electromigration* of NaCl in a Brinkman medium with charged spherical inclusions (see Hill 2006c, for details): $\ell/a = 0.1$ ($a = 10$ nm, $\ell = 1$ nm); $T = 25^\circ\text{C}$; $D_1 \approx 1.33 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ (Na^+); $D_2 \approx 2.03 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ (Cl^-); $u^* = \epsilon_s \epsilon_o (kT/e)^2 / (\eta a) \approx 5.15 \times 10^{-2} \text{ m s}^{-1}$.

$\zeta e/(kT)$	D^E/a^3	$C_j^E kT/(2Ia^3 e)$ ($j = 1, 2$)	$C^E kT/(u^* a^4 e)$	ΔK	Δ_1^E	Δ_2^E	$-3C^E/a^3$ [(nm s ⁻¹)/(V cm ⁻¹)]
$\kappa a = 0.1, I = 9.25 \times 10^{-6} \text{ mol l}^{-1}$							
-1.0 ⁻⁶	-4.999 ⁻¹	5.505 ⁻⁵	-4.396 ⁻⁸	-1.499 ⁺⁰	-1.499 ⁺⁰	-1.500 ⁺⁰	2.644 ⁻⁴
-0.5	-2.825 ⁻¹	2.752 ⁺¹	-2.197 ⁻²	-3.517 ⁺¹	1.642 ⁺²	-1.659 ⁺²	1.322 ⁺²
-1.0	3.664 ⁻¹	5.500 ⁺¹	-4.391 ⁻²	-6.751 ⁺¹	3.310 ⁺²	-3.288 ⁺²	2.641 ⁺²
-2.0	2.912 ⁺⁰	1.096 ⁺²	-8.752 ⁻²	-1.280 ⁺²	6.665 ⁺²	-6.491 ⁺²	5.265 ⁺²
-4.0	1.232 ⁺¹	2.162 ⁺²	-1.724 ⁻¹	-2.327 ⁺²	1.334 ⁺³	-1.260 ⁺³	1.037 ⁺³
-6.0	2.544 ⁺¹	3.148 ⁺²	-2.507 ⁻¹	-3.164 ⁺²	1.965 ⁺³	-1.812 ⁺³	1.508 ⁺³
$\kappa a = 1, I = 9.25 \times 10^{-4} \text{ mol l}^{-1}$							
-1.0 ⁻⁶	-4.999 ⁻¹	1.047 ⁻⁶	-7.615 ⁻⁸	-1.499 ⁺⁰	-1.499 ⁺⁰	-1.499 ⁺⁰	4.581 ⁻⁴
-0.5	-4.690 ⁻¹	5.232 ⁻¹	-3.797 ⁻²	-2.059 ⁺⁰	1.688 ⁺⁰	-4.517 ⁺⁰	2.284 ⁺²
-1.0	-3.782 ⁻¹	1.041 ⁺⁰	-7.536 ⁻²	-2.434 ⁺⁰	5.028 ⁺⁰	-7.327 ⁺⁰	4.534 ⁺²
-2.0	-4.340 ⁻²	2.043 ⁺⁰	-1.459 ⁻¹	-2.679 ⁺⁰	1.196 ⁺¹	-1.227 ⁺¹	8.781 ⁺²
-4.0	9.125 ⁻¹	3.735 ⁺⁰	-2.548 ⁻¹	-1.921 ⁺⁰	2.485 ⁺¹	-1.947 ⁺¹	1.533 ⁺³
-6.0	1.666 ⁺⁰	4.793 ⁺⁰	-3.080 ⁻¹	-9.797 ⁻¹	3.340 ⁺¹	-2.352 ⁺¹	1.853 ⁺³
$\kappa a = 10, I = 9.25 \times 10^{-2} \text{ mol l}^{-1}$							
-1.0 ⁻⁶	-4.999 ⁻¹	7.197 ⁻⁸	-2.194 ⁻⁷	-1.499 ⁺⁰	-1.499 ⁺⁰	-1.499 ⁺⁰	1.320 ⁻³
-0.5	-4.914 ⁻¹	3.640 ⁻²	-1.092 ⁻¹	-1.519 ⁺⁰	-1.382 ⁺⁰	-1.609 ⁺⁰	6.574 ⁺²
-1.0	-4.658 ⁻¹	7.435 ⁻²	-2.158 ⁻¹	-1.490 ⁺⁰	-1.201 ⁺⁰	-1.679 ⁺⁰	1.298 ⁺³
-2.0	-3.663 ⁻¹	1.581 ⁻¹	-4.088 ⁻¹	-1.296 ⁺⁰	-6.239 ⁻¹	-1.737 ⁺⁰	2.459 ⁺³
-4.0	-4.427 ⁻²	3.505 ⁻¹	-6.307 ⁻¹	-5.701 ⁻¹	1.239 ⁺⁰	-1.756 ⁺⁰	3.794 ⁺³
-6.0	2.307 ⁻¹	5.035 ⁻¹	-6.172 ⁻¹	6.402 ⁻²	2.997 ⁺⁰	-1.859 ⁺⁰	3.713 ⁺³
$\kappa a = 100, I = 9.25 \times 10^{+0} \text{ mol l}^{-1}$							
-1.0 ⁻⁶	-4.999 ⁻¹	7.895 ⁻⁹	-3.362 ⁻⁷	-1.499 ⁺⁰	-1.499 ⁺⁰	-1.499 ⁺⁰	2.023 ⁻³
-0.5	-4.985 ⁻¹	3.825 ⁻³	-1.679 ⁻¹	-1.500 ⁺⁰	-1.667 ⁺⁰	-1.390 ⁺⁰	1.010 ⁺³
-1.0	-4.941 ⁻¹	8.098 ⁻³	-3.349 ⁻¹	-1.492 ⁺⁰	-1.822 ⁺⁰	-1.276 ⁺⁰	2.014 ⁺³
-2.0	-4.754 ⁻¹	1.940 ⁻²	-6.604 ⁻¹	-1.450 ⁺⁰	-2.075 ⁺⁰	-1.040 ⁺⁰	3.973 ⁺³
-4.0	-3.852 ⁻¹	6.369 ⁻²	-1.214 ⁺⁰	-1.235 ⁺⁰	-2.181 ⁺⁰	-6.149 ⁻¹	7.304 ⁺³
-6.0	-2.108 ⁻¹	1.493 ⁻¹	-1.456 ⁺⁰	-8.190 ⁻¹	-1.425 ⁺⁰	-4.213 ⁻¹	8.765 ⁺³



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TABLE II

Scaled (dimensionless) asymptotic coefficients for bulk diffusion of NaCl in a Brinkman medium charged spherical inclusions (see Hill 2006b, for details): $\ell/a = 0.1$ ($a = 10$ nm, $\ell = 1$ nm); $T = 298$ K; $D_1 \approx 1.33 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ (Na^+); $D_2 \approx 2.03 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ (Cl^-); $u^* = \epsilon_s \epsilon_o (kT/e)^2 / (\eta a) \approx 5.15 \times 10^{-2} \text{ m}^2 \text{ s}^{-1}$

$\zeta e/(kT)$	$D^B 2Ie/(kTa^3)$	C_j^B/a^3 ($j = 1, 2$)	$C^B 2I/(u^* a^4)$	$-3C^B/a^3$ [(nm s ⁻¹)/(mol l ⁻¹ cm ⁻¹)]	$3D^B/a^3$ (V/mol l ⁻¹)	Δ_1^B	Δ_2^B
$\kappa a = 0.1, I = 9.25 \times 10^{-6} \text{ mol l}^{-1}$							
-1.0 ⁻⁶	-2.202 ⁻⁴	4.999 ⁻¹	6.473 ⁻¹⁶	-5.406 ⁻⁹	-9.171 ⁻¹	-1.499 ⁺⁰	-1.500 ⁺⁰
-0.5	-1.100 ⁺²	2.826 ⁻¹	1.615 ⁻⁴	-1.349 ⁺³	-4.584 ⁺⁵	1.642 ⁺²	-1.650 ⁺²
-1.0	-2.199 ⁺²	-3.660 ⁻¹	6.425 ⁻⁴	-5.366 ⁺³	-9.162 ⁺⁵	3.310 ⁺²	-3.280 ⁺²
-2.0	-4.386 ⁺²	-2.911 ⁺⁰	2.512 ⁻³	-2.098 ⁺⁴	-1.826 ⁺⁶	6.666 ⁺²	-6.490 ⁺²
-4.0	-8.648 ⁺²	-1.231 ⁺¹	9.136 ⁻³	-7.630 ⁺⁴	-3.601 ⁺⁶	1.334 ⁺³	-1.260 ⁺³
-6.0	-1.259 ⁺³	-2.543 ⁺¹	1.713 ⁻²	-1.431 ⁺⁵	-5.245 ⁺⁶	1.965 ⁺³	-1.810 ⁺³
$\kappa a = 1, I = 9.25 \times 10^{-4} \text{ mol l}^{-1}$							
-1.0 ⁻⁶	-4.191 ⁻⁶	4.999 ⁻¹	4.276 ⁻¹⁵	-3.571 ⁻¹⁰	-1.745 ⁻⁴	-1.499 ⁺⁰	-1.499 ⁺⁰
-0.5	-2.092 ⁺⁰	4.699 ⁻¹	1.054 ⁻³	-8.807 ⁺¹	-8.714 ⁺¹	1.728 ⁺⁰	-4.540 ⁺⁰
-1.0	-4.165 ⁺⁰	3.816 ⁻¹	4.046 ⁻³	-3.380 ⁺²	-1.734 ⁺²	5.100 ⁺⁰	-7.350 ⁺⁰
-2.0	-8.165 ⁺⁰	5.620 ⁻²	1.370 ⁻²	-1.144 ⁺³	-3.400 ⁺²	1.207 ⁺¹	-1.240 ⁺¹
-4.0	-1.490 ⁺¹	-8.713 ⁻¹	2.938 ⁻²	-2.454 ⁺³	-6.208 ⁺²	2.495 ⁺¹	-1.970 ⁺¹
-6.0	-1.911 ⁺¹	-1.604 ⁺⁰	3.105 ⁻²	-2.593 ⁺³	-7.961 ⁺²	3.346 ⁺¹	-2.380 ⁺¹
$\kappa a = 10, I = 9.25 \times 10^{-2} \text{ mol l}^{-1}$							
-1.0 ⁻⁶	-2.881 ⁻⁷	4.999 ⁻¹	-6.007 ⁻¹⁵	5.017 ⁻¹²	-1.200 ⁻⁷	-1.499 ⁺⁰	-1.499 ⁺⁰
-0.5	-1.445 ⁻¹	4.934 ⁻¹	-1.440 ⁻³	1.203 ⁺⁰	-6.018 ⁻²	-1.262 ⁺⁰	-1.690 ⁺⁰
-1.	-2.919 ⁻¹	4.739 ⁻¹	-5.097 ⁻³	4.257 ⁺⁰	-1.215 ⁻¹	-9.810 ⁻¹	-1.850 ⁺⁰
-2.0	-6.046 ⁻¹	3.981 ⁻¹	-1.273 ⁻²	1.063 ⁺¹	-2.518 ⁻¹	-2.800 ⁻¹	-2.090 ⁺⁰
-4.0	-1.295 ⁺⁰	1.396 ⁻¹	-8.868 ⁻³	7.407 ⁺⁰	-5.394 ⁻¹	1.529 ⁺⁰	-2.350 ⁺⁰
-6.0	-1.892 ⁺⁰	-1.239 ⁻¹	3.962 ⁻⁴	-3.309 ⁻¹	-7.880 ⁻¹	3.210 ⁺⁰	-2.460 ⁺⁰
$\kappa a = 100, I = 9.25 \times 10^{+0} \text{ mol l}^{-1}$							
-1.0 ⁻⁶	-2.829 ⁻⁸	4.999 ⁻¹	-1.991 ⁻¹⁴	1.663 ⁻¹³	-1.178 ⁻¹⁰	-1.499 ⁺⁰	-1.499 ⁺⁰
-0.5	-1.499 ⁻²	4.990 ⁻¹	-4.801 ⁻³	4.010 ⁻²	-6.244 ⁻⁵	-1.471 ⁺⁰	-1.510 ⁺⁰
-1.0	-3.076 ⁻²	4.963 ⁻¹	-1.729 ⁻²	1.444 ⁻¹	-1.281 ⁻⁴	-1.432 ⁺⁰	-1.520 ⁺⁰
-2.0	-6.812 ⁻²	4.848 ⁻¹	-4.765 ⁻²	3.980 ⁻¹	-2.837 ⁻⁴	-1.324 ⁺⁰	-1.530 ⁺⁰
-4.0	-1.958 ⁻¹	4.280 ⁻¹	-6.521 ⁻²	5.447 ⁻¹	-8.155 ⁻⁴	-9.525 ⁻¹	-1.550 ⁺⁰
-6.0	-4.487 ⁻¹	3.043 ⁻¹	-4.797 ⁻²	4.007 ⁻¹	-1.868 ⁻³	-2.119 ⁻¹	-1.560 ⁺⁰

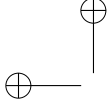
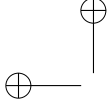


TABLE III

Scaled (dimensionless) asymptotic coefficients for bulk convection of NaCl in a Brinkman medium with charged spherical inclusions (see Hill 2006c, for details): $\ell/a = 0.1$ ($a = 10$ nm, $\ell = 1$ nm); $T = 25^\circ\text{C}$, $D_1 \approx 1.33 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ (Na^+); $D_2 \approx 2.03 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ (Cl^-); $u^* = \epsilon_s \epsilon_o (kT/e)^2 / (\eta a) \approx 5.15 \times 10^{-2} \text{ m s}^{-1}$.

$\zeta e / (kT)$	$D^U e u^* / (kT a^2)$	$C_j^U u^* / (2I a^2)$ ($j = 1, 2$)	C^U / a^3
$\kappa a = 0.1, I = 9.25 \times 10^{-6} \text{ mol l}^{-1}$			
-1.0^{-6}	3.515^{-5}	3.654^{-6}	8.599^{-1}
-0.5	1.758^{+1}	1.859^{+0}	8.599^{-1}
-1.0	3.517^{+1}	3.779^{+0}	8.600^{-1}
-2.0	7.021^{+1}	7.783^{+0}	8.607^{-1}
-4.0	1.386^{+2}	1.621^{+1}	8.633^{-1}
-6.0	2.020^{+2}	2.457^{+1}	8.698^{-1}
$\kappa a = 1, I = 9.25 \times 10^{-4} \text{ mol l}^{-1}$			
-1.0^{-6}	6.090^{-7}	6.331^{-8}	8.599^{-1}
-0.5	3.049^{-1}	3.442^{-2}	8.601^{-1}
-1.0	6.074^{-1}	7.375^{-2}	8.605^{-1}
-2.0	1.184^{+0}	1.610^{-1}	8.624^{-1}
-4.0	2.087^{+0}	3.131^{-1}	8.688^{-1}
-6.0	2.539^{+0}	3.684^{-1}	8.733^{-1}
$\kappa a = 10, I = 9.25 \times 10^{-2} \text{ mol l}^{-1}$			
-1.0^{-6}	1.754^{-8}	1.824^{-9}	8.599^{-1}
-0.5	8.824^{-3}	1.096^{-3}	8.599^{-1}
-1.0	1.762^{-2}	2.527^{-3}	8.600^{-1}
-2.0	3.424^{-2}	5.999^{-3}	8.601^{-1}
-4.0	5.657^{-2}	1.131^{-2}	8.605^{-1}
-6.0	5.854^{-2}	9.734^{-3}	8.608^{-1}
$\kappa a = 100, I = 9.25 \times 10^{+0} \text{ mol l}^{-1}$			
-1.0^{-6}	2.689^{-10}	2.795^{-11}	8.599^{-1}
-0.5	1.360^{-4}	1.794^{-5}	8.599^{-1}
-1.0	2.747^{-4}	4.359^{-5}	8.599^{-1}
-2.0	5.566^{-4}	1.152^{-4}	8.599^{-1}
-4.0	1.091^{-3}	3.016^{-4}	8.599^{-1}
-6.0	1.434^{-3}	4.393^{-4}	8.599^{-1}



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($a = 100$ nm and $\ell \approx 1$ nm) (Hill 2006c, a). This difference affects all quantities derived from the microscale analysis that depend on convective flow³.

STREAMING POTENTIAL

A fundamental characteristic of interest that has not been explicitly considered for hydrogel-colloidal composites is the streaming potential. This is the differential potential $\Delta\langle\psi\rangle$ that prevails when $\Delta\langle n\rangle = 0$ with $u \neq 0$ and $\Delta\langle p\rangle \neq 0$. Accordingly, when $\phi \ll 1$, the streaming potential is

$$\Delta\langle\psi\rangle = -\Delta\langle p\rangle(\ell^2/\eta)(3\phi/a^3) \left[D^U + \frac{(\gamma-1)kT}{(\gamma z_1 - z_2)e\langle n\rangle} C_j^U \right],$$

where, recall, $\gamma = D_1/D_2$. This equation is obtained by multiplying Eqn. (23) for each species and setting their sum (electrical current) to zero. Note that terms involving the product $\phi\langle\nabla\psi\rangle$ are smaller than the electromigrative term for the pure electrolyte, and a consistent approximation of Eqn. (23) is $u \approx -(\ell^2/\eta)\Delta\langle p\rangle/L$, since $\phi \ll 1$.

Writing Eqn. (39) in terms of the dimensionless asymptotic coefficients provided in Table 3 above

$$\Delta\langle\psi\rangle = -\frac{3\phi\Delta\langle p\rangle\ell^2 e}{\epsilon_o\epsilon_s kT} \left[\overline{D}^U + \frac{2(\gamma-1)}{(\gamma z_1 - z_2)} \overline{C}_j^U \right],$$

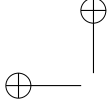
where $\overline{D}^U \equiv D^U e u^*/(kT a^2)$ and $\overline{C}_j^U \equiv C_j^U u^*/(2I a^2)$ with $u^* = \epsilon_o\epsilon_s(kT/e)^2/(\eta a)$. Note that $\langle n\rangle$ is the bulk ionic strength. Equation (40) reveals that very large pressure differentials ($\sim 10^5$ Pa) are needed to produce even small streaming potentials (~ 1 mV). In general, therefore, the streaming potential is not a practically viable means of probing the microstructure.

CONCENTRATION-GRADIENT DRIVEN FLUX WITH ZERO ELECTRICAL CURRENT AND FLOW

In the following example, the flux is specified as $j = -D^e[\langle n\rangle(L) - \langle n\rangle(0)]$ [Eqn (15)], with $\langle n\rangle(0) = 0.01$ mmol l⁻¹, $\langle n\rangle(L) = 10$ mmol l⁻¹ and $L = 500$ μ m, so $\Delta \ln \langle n\rangle \approx 6.9$. Recall, this flux prevails in the absence of charged inclusions when $u = 0$. The electrical current density $i = 0$, so $j_1 = j_2$. Note that the numerically exact solutions do not yield $\langle n\rangle(x = L) = 10$ mmol l⁻¹, because the charged inclusions affect the macroscale fluxes. Also, while the calculations could be performed with $\Delta\langle p\rangle = 0$ and, hence, $u = 0$, for simplicity the computations were undertaken with $u = 0$, so $\Delta\langle p\rangle \neq 0$. The asymptotic coefficients are determined by the local bulk electrolyte concentration. Accordingly, from the local values of κa and $\zeta e/kT$, asymptotic coefficients are obtained by interpolating refined versions of Tables I, II and III. In the following, the results of the microscale calculations, and a discussion of various quantities derived from them, are given by Hill (2006a, c).

When $\Delta \ln \langle n\rangle \ll 1$, it is reasonable to approximate the asymptotic coefficients as constants based on an approximately constant bulk concentration $\langle n\rangle$, so

$$\frac{\Delta\langle\psi\rangle}{\Delta \ln \langle n\rangle} \approx \frac{(kT/e) \frac{(1-\gamma)}{(\gamma z_1 - z_2)} + (3\phi/a^3) \left[\langle n\rangle D^B - (kT/e) \frac{(1-\gamma)}{(\gamma z_1 - z_2)} C_j^B \right]}{1 + (2\phi/a^3) \left[D^B + \frac{(1-\gamma)}{(\gamma z_1 - z_2)} C_j^B \right]},$$



where, recall, $\gamma = D_1/D_2$, $i = u = 0$, and $\phi \ll 1$. Again, this equation is obtained by multiplying Eqn. (23) for each species by $z_j e$ and setting their sum (electrical current) to zero; note also that $\Delta \langle n \rangle / L \approx (\langle n \rangle / L) \Delta \ln \langle n \rangle$. Writing Eqn. (41) in terms of the dimensionless asymptotic coefficients provided in Tables I and II gives

$$\frac{\Delta \langle \psi \rangle e / (kT)}{\Delta \ln \langle n \rangle} \approx \frac{\frac{(1-\gamma)}{(\gamma z_1 - z_2)} + 3\phi \left[\bar{D}^B / 2 - \frac{(1-\gamma)}{(\gamma z_1 - z_2)} \bar{C}_j^B \right]}{1 + 3\phi \left[\bar{D}^E + \frac{2(1-\gamma)}{(\gamma z_1 - z_2)} \bar{C}_j^E \right]} \quad (42)$$

or

$$\frac{\Delta \langle \psi \rangle e / (kT)}{\Delta \ln \langle n \rangle} \frac{(\gamma z_1 - z_2)}{(1 - \gamma)} \approx 1 + 3\phi \left[\frac{(\gamma z_1 - z_2)}{2(1 - \gamma)} \bar{D}^B - \bar{C}_j^B - \bar{D}^E - \frac{2(1 - \gamma)}{(\gamma z_1 - z_2)} \bar{C}_j^E \right], \quad (43)$$

where $\bar{D}^B \equiv D^B 2Ie / (kTa^3)$, $\bar{C}_j^B \equiv C_j^B / a^3$, $\bar{D}^E \equiv D^E / a^3$ and $\bar{C}_j^E \equiv C_j^E kT / (2Ia^3 e)$, with $u^* = \epsilon_o \epsilon_s (kT/e)^2 / (\eta a)$. Note that $\langle n \rangle = I$ (bulk ionic strength), and that the increment

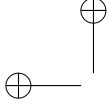
$$\begin{aligned} \Delta^E &\equiv [\langle \psi \rangle(x = L; \phi = 0) / \langle \psi \rangle(x = L; \phi) - 1] / \phi \\ &\approx 3 \left[\frac{(\gamma z_1 - z_2)}{2(1 - \gamma)} \bar{D}^B - \bar{C}_j^B - \bar{D}^E - \frac{2(1 - \gamma)}{(\gamma z_1 - z_2)} \bar{C}_j^E \right] \end{aligned} \quad (44)$$

is the same as the more general expression of Hill (2006b). Furthermore, a careful inspection of Tables I and II reveals that the dimensionless asymptotic coefficients generally yield $\phi \Delta^E \sim 1$ only when $\kappa a < 1$ and $|\zeta| > kT/e$.

Note that microscale theory does not account for particle interactions, so $\phi^* = \phi[1 + (\kappa a)^{-1}]^3$ should be small. This is restrictive on the particle volume fraction $\phi = c(4/3)\pi a^3$ when $\kappa a \ll 1$ (c is the particle number density). For the specific example introduced above with $\Delta \ln \langle n \rangle \approx 6.9$, the macroscale calculations were undertaken with $\phi = 0.64(0, 0.1, 0.2, 0.4, 0.8) / [1 + (\kappa a)^{-1}]^3$, with $\kappa a < 1$ evaluated at $x = 0$, which is generally the position where the ionic strength is lowest (with $j > 0$) and, hence, where κa is smallest. With $\langle n \rangle(0) = 0.01 \text{ mmol l}^{-1}$, $\phi \approx (0, 0.0534, 0.1069, 0.2137, 0.4275) \times 10^{-3}$. Note also that calculations were performed with a constant particle surface charge density $\sigma = 1 \mu\text{C cm}^{-2}$, with the ζ -potential varying according to the (semi-empirical) formula (Russel et al. 1989)

$$\sigma = \epsilon_o \epsilon_s [kT / (ze)] \kappa \{ 2 \sinh [\zeta ze / (2kT)] + [4 / (\kappa a)] \tanh [\zeta ze / (4kT)] \}. \quad (45)$$

When $\phi = 0$, the bulk concentration varies approximately linearly across the membrane, as given by Eqn. (15) when $\text{Pe} \rightarrow 0$. As the inclusion volume fraction increases, the specified flux j is achieved with practically the same (almost uniform) electrolyte concentration gradient, even though the membrane is macroscopically inhomogeneous due to the varying ζ -potential. As seen in Figure 1, the high surface charge density and low bulk electrolyte concentration produce a high ζ -potential at $x = 0$. With higher electrolyte concentrations, the ζ -potentials are low (with fixed surface charge) and the diffuse double layers thin; accordingly, the inclusions behave as impenetrable uncharged spheres and the membrane potential tends to its value for pure electrolyte, and the effective diffusion coefficients tend to their Maxwell values (see below). These and other limiting cases were thoroughly discussed by Hill (2006b, c).



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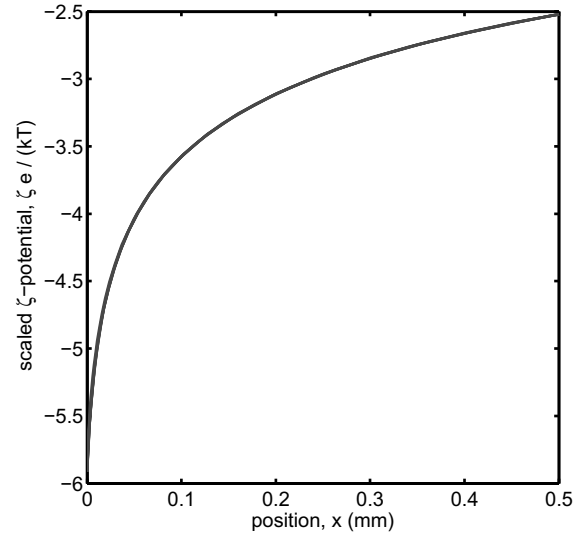


Fig. 1 – Scaled particle ζ -potential $\zeta e/(kT)$ according to Eqn. (45) ($a = 10$ nm) as a function of position x (mm) with particle surface charge density $\sigma = 1 \mu\text{C cm}^{-2}$. The accompanying bulk ionic strength varies approximately linearly with position: $\langle I \rangle \approx 0.01 + (10 - 0.01)(x/L) \text{ mmol l}^{-1}$.

Increasing the particle concentration decreases the membrane potential $\Delta\langle\psi\rangle = \langle\psi\rangle(x = L)$. At the highest particle concentration of only $\phi \approx 4 \times 10^{-4}$, $\Delta\langle\psi\rangle$ is about 20 mV *lower* than in the absence of inclusions. From Eqn. (20), $\Delta\langle\psi\rangle \approx 24.6$ mV. Therefore, the increment $\Delta^E \equiv [\langle\psi\rangle(x = L) - \langle\psi\rangle(x = 0)]/\langle\psi\rangle(x = L; \phi) \sim -10^3$, which is in good agreement with expectations for uniform membranes with small macroscale gradients (Hill 2006c, Fig. 7).

As identified by Hill (2006c), the negatively charged inclusions here with Na^+ counterion reduce the effective asymmetry of the electrolyte by increasing (decreasing) the effective diffusion coefficient of the otherwise less (more) mobile Na^+ (Cl^-) ion. This diminishes the accompanying electric field required to maintain equal bulk fluxes (zero electrical current). The bottom panel of Figure 2 shows the electrostatic potential for membranes with the same particle volume fractions and electrolyte, but with constant particle ζ -potential ($\zeta = -4kT/e \approx -100$ mV) rather than constant surface charge. In both cases, the gradient of the electrostatic potential is negative in a thin region at $x = 0$. In the absence of an accompanying pressure gradient, the large, positive electric field would drive electroosmotic flow in the direction of the concentration gradient (from left to right). However, because these calculations have been performed with zero convective flow ($u = 0$), the pressure, which is plotted in Figure 3, varies in a very similar manner to the electrostatic potential.

A useful measure of the overall influence of the inclusions on transport is the bulk diffusion coefficient

$$D^* \equiv -jx/[\langle n \rangle(x) - \langle n \rangle(0)].$$

This is plotted in Figure 4 scaled with the diffusion coefficient D^e given by Eqn. (17) for electrodiffusion.

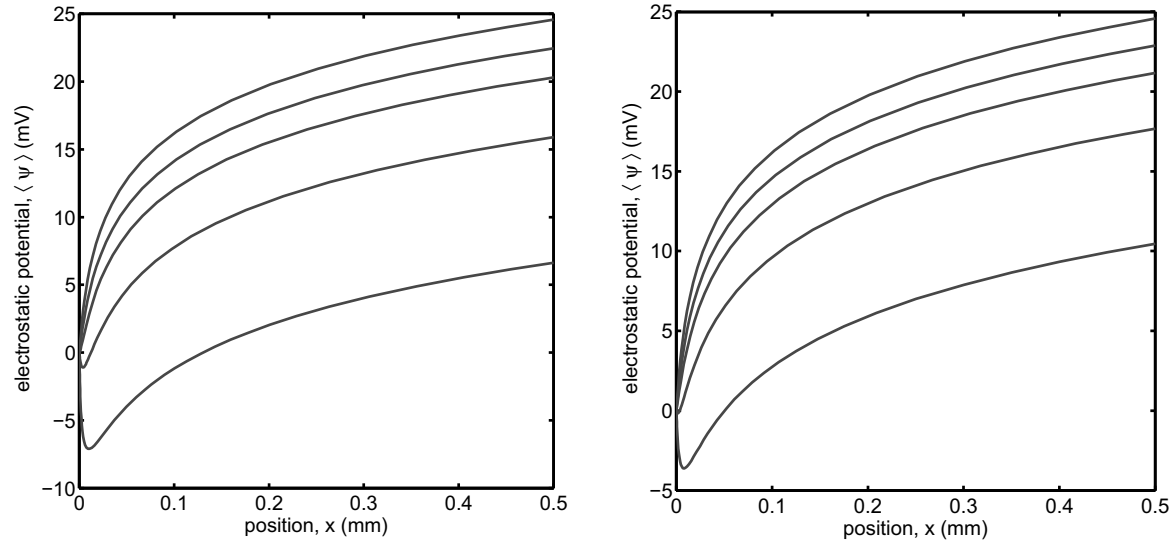
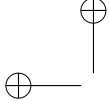


Fig. 2 – Bulk electrostatic potential $\langle \psi \rangle$, scaled with $kT/e \approx 25$ mV, as a function of position x (mm), decreasing monotonically with increasing particle volume fraction $\phi = \phi^*(0, 0.1, 0.2, 0.4, 0.8) = (0, 0.0534, 0.1069, 0.2137, 0.4275) \times 10^{-3}$: constant charge density $\sigma = 1 \mu\text{C cm}^{-2}$ (left panel); constant ζ -potential $\zeta = -4kT/e \approx -100$ mV (right panel). The accompanying bulk electrolyte concentration gradient is practically constant. See text and Tables I–III for other microscale parameters.

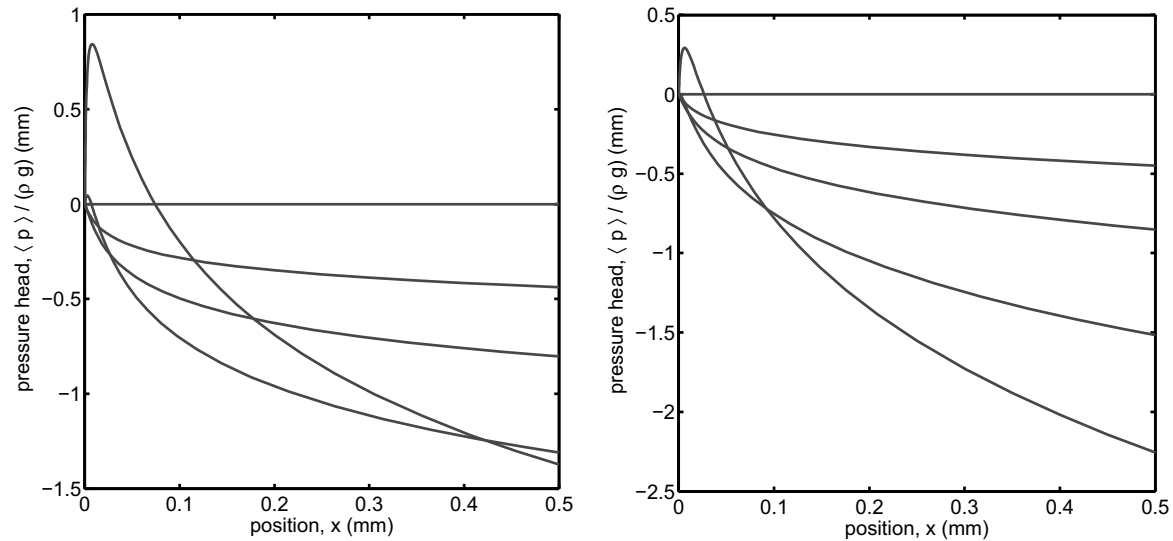
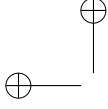


Fig. 3 – Bulk pressure head $\langle p \rangle / (\rho g)$ (mm) as a function of position x (mm), decreasing monotonically at $x = L$ with increasing particle volume fraction $\phi = \phi^*(0, 0.1, 0.2, 0.4, 0.8) = (0, 0.0534, 0.1069, 0.2137, 0.4275) \times 10^{-3}$: constant charge density



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diffusion coefficient of a tracer in a dilute random array of impenetrable spherical inclusions is (Mason 1873, Batchelor and O’Brien 1977)⁴

$$D^* = D[1 - (3/2)\phi],$$

so with the largest value of $\phi \approx 0.000428$, Eqn. (47) gives $D^*/D \approx 0.9994$. However, the top panel of Figure 4 indicates that $D^*/D^e \approx 1.0030$ when $\phi = 0.000428$, so, overall, the charge on the inclusions produces a *higher* effective diffusivity than expected from Eqn. (47).

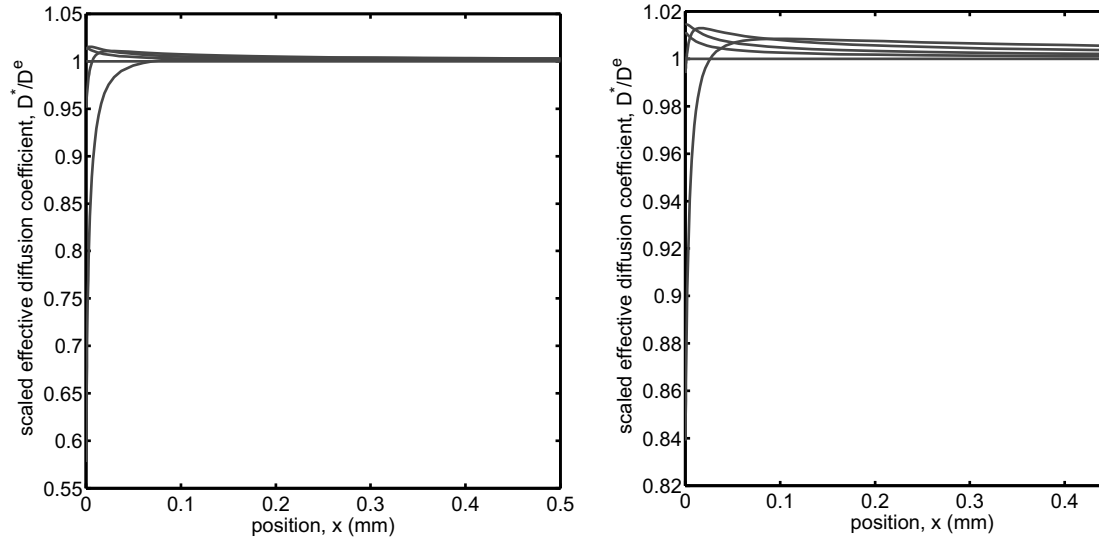
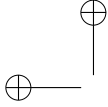


Fig. 4 – Bulk diffusion constant $D^* \equiv -jx/[\langle n \rangle(x) - \langle n \rangle(0)]$ scaled with $D^e \equiv 2/[1/D_1 + 1/D_2]$ [Eqn. (17)] as a function of position x (mm), decreasing monotonically at $x = L$ with increasing particle volume fraction $\phi = \phi^*(0, 0.1, 0.2, 0.4) \times 10^{-3}$ (0, 0.0534, 0.1069, 0.2137, 0.4275) $\times 10^{-3}$: constant charge density $\sigma = 1 \mu\text{C cm}^{-2}$ (left panel); constant ζ -potential $-4kT/e \approx -100$ mV (right panel). The accompanying bulk electrolyte concentration gradient is practically constant. See Tables I–III for other microscale parameters.

The overall, but very slight, increase in the flux due to the inclusions is more pronounced in the bottom panel of Figure 4, because the particle ζ -potential ($\zeta \approx -100$ mV) is relatively high and uniform throughout the membrane; for example, $D^*(L)/D^e \approx 1.0055$ when $\phi \approx 0.000428$. Here the incremental quantity $[D^*(L)/D^e - 1]/\phi \sim 10$. This is much greater than the value $-3/2$ from Eqn. (47), but comparable with expectations for uniform composites with small macroscale gradients (Hill 2006b). For example, incremental contributions to the individual ion diffusion coefficients in Table II (Δ_1^B for Na^+ and Δ_2^B for Cl^-) (see also Hill 2006b, Fig. 6) reveal that the inclusions increase (decrease) the effective diffusion coefficient of the otherwise less (more) mobile Na^+ (Cl^-) ion. Accordingly, the negatively charged inclusions *decrease* the asymmetry of the NaCl electrolyte, which explains the overall decrease in the membrane potential shown in Figure 1. It is also evident from Table II that when $\zeta e/(kT)$ is large, the inclusions enter the effective diffusion of Na^+ and Cl^- ions at $\Delta_1^B/\Delta_2^B \approx 1$. This explains the small



for $D^*(L)/D^e$ to be greater than one. Clearly, lower ζ -potentials will yield $D^*(L)/D^e$ less than one, as expected from Eqn. (47) when $\zeta \rightarrow 0$.

SUMMARY

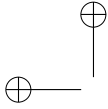
Numerical solutions of the coupled macroscale ion conservation equations and fluid mass and momentum conservation equations for electrodifusion across hydrogel-colloid composite membranes were presented for the first time. These computations were undertaken with the approximation of local macroscale electroneutrality, using bulk transport properties established in earlier work for microscale electrokinetic transport processes. The principal example presented was characterized by a low bulk electrolyte concentration on one side of the membrane, with a very low solid volume fraction of small, highly charged colloidal inclusions. The influence of these inclusions on the bulk fluxes was negligible in absolute terms, but the incremental contribution of the particles was significantly larger than expected from Maxwell’s classical theory for impenetrable particles in a permeable continuum. Significant from a practical perspective was that very low concentrations of inclusions have a measurable impact on the membrane diffusion potential. Such changes reflect the size, charge, and concentration of the inclusions. Therefore, experimental measurements of the membrane potential may be promising for testing the microscale theory, which underlies several other interesting and technologically important microscale electrokinetic problems, including those of electrical microrheology and electroacoustics.

ACKNOWLEDGMENTS

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RESUMO

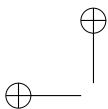
Um modelo eletrocinético rigoroso para compósitos formados por um hidrogel e um colóide é adotado para computar os perfis macroscópicos de concentração eletrolítica, potencial eletrostático e pressão hidrostática através de uma membrana que separa soluções com diferentes concentrações eletrolíticas. A membrana é composta por um hidrogel polimérico sem carga elétrica onde partículas esféricas são imobilizadas e dispersas aleatoriamente com baixa fração de volume do sólido. As características da membrana e a sua performance são calculadas a partir de um modelo eletrocinético de contínuo microscópico (Hill 2006b, c). As computações realizadas neste artigo quantificam os potenciais de corrente e de membrana. Para o potencial de membrana, aumentando a fração de volume das inclusões carregadas negativamente diminui o diferencial do potencial eletrostático através da membrana sob condições de fluxo convectivo e corrente elétrica nulos. Para concentrações eletrolíticas baixas o potencial de membrana torna-se muito sensível à fração de volume das partículas. De maneira similar, o potencial de membrana e as cargas elétricas trazidos pelo tamanho da inclusão, carga e concentração podem prover um diagnóstico experimental útil para complementar aplicações mais recentes do modelo eletrocinético microscópico em eletroacústica e eletro-micro-reologia (Hill and



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