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ADSORPTION KINETICS OF N₂O ON NATURAL ZEOLITES

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Key words: adsorption rate, erionite, mordenite, clinoptilolite

ABSTRACT

The adsorption kinetics of pure N₂O on natural zeolites of the erionite (ZAPS), mordenite (ZNT), and clinoptilolite (ZSL) types has been measured in the temperature range of 0-100 °C using a glass, high-vacuum volumetric system. The adsorption capacities of N₂O on the ZNT and ZSL samples were lower than that on ZAPS. This result can be due to the limiting volume of the micropores of these zeolites and to the quantity of cations available per unit mass of the dehydrated zeolites (cationic density). It was found that the adsorbed amount and the adsorption rate diminish with increasing temperature. This behavior allows us to deduce that the adsorption process of N₂O is not of the activated type and that it is not influenced by kinetic effects. It was established that the adsorption of N₂O on ZAPS can be effected most efficiently at ambient temperature, whereas the use of ZSL could be recommended at 100 °C.

Palabras clave: velocidad de adsorción, erionita, mordenita, clinoptilolita

RESUMEN

Se estudio la cinética de adsorción del N₂O en tres zeolitas naturales tipo erionita (ZAPS), mordenita (ZNT) y clinoptilolita (ZSL) a una temperatura de 0 a 100 °C en un sistema volumétrico al alto vacío. Las cantidades de adsorción de N₂O en las muestras ZNT y ZSL son más bajos que en la ZAPS. Este resultado puede ser debido a la limitación de volumen de los microporos de estas zeolitas y a la cantidad de cationes disponibles por unidad de masa de las zeolitas deshidratadas (densidad de cationes). Se encontró que la cantidad adsorbida y la velocidad de adsorción disminuyen al aumentar la temperatura. Este comportamiento nos permite deducir que el proceso de adsorción de N₂O es del tipo no activado y por lo tanto no está influenciado por efectos cinéticos. Se estableció que la adsorción de N₂O en ZAPS puede efectuarse de manera más eficiente a temperatura ambiente, mientras que el uso de la ZSL se recomienda a 100 °C.

INTRODUCTION

The nitrogen oxides in the atmosphere contribute to the formation of photochemical smog and of acid rain precursors, to the destruction of ozone in the stratosphere, and to global warming (Kapteijn *et al.* 1997). Over the past 150 years, global emissions of nitrogen oxides into the atmosphere have been increasing steadily. A significant amount of the nitrogen oxide emissions is attributed to the combustion of biomass and fossil fuels. Increasingly stringent NO_x emission regulations are being implemented in a number of industrialized countries. These regulations have driven the development of NO_x emission control techniques (Wu *et al.* 2015).

An alternative process for the elimination of nitrogen oxides is the adsorption of these gases onto porous adsorbent materials. This method allows the separate adsorption and subsequent desorption of these gases at different temperatures for their treatment or direct application (Longhurst *et al.* 1993, Kohl *et al.* 1997). Pure N₂O is used, for example, for oxidation reactions (Centi *et al.* 2000), whereas NO is used as a crucial biological agent in the cardiovascular, nervous, and immune systems (Wheatley *et al.* 2006).

Natural zeolites may be used because they have a porous structure with high-volume pores where nitrogen oxides could be adsorbed. Also, zeolites can be modified by cation exchange and cations provide active sites that enhance selective adsorption (Centi *et al.* 2000).

Studies of the adsorption of oxides on synthetic zeolites have already been performed. However, the study of adsorption on natural zeolites is still a non-explored field. Therefore, the main objective of this work was to study the adsorption kinetics of pure N₂O on three Mexican natural zeolites at different temperatures and to use the results obtained to find a suitable adsorbent.

MATERIALS AND METHODS

Three natural zeolites of the erionite (ZAPS), morденite (ZNT), and clinoptilolite (ZSL) types, from various deposits in Mexico were used. N₂O was provided by INFRA (CP grade) with a minimum purity of 99.0 % and was used without further purification.

Characterization of the adsorbents

The adsorbents were characterized using the adsorption of N₂ at 77 K. The results obtained were reported in previous studies (Hernández-Huesca *et al.* 1999).

Adsorption kinetics measurement

Adsorption kinetic uptake was measured using a conventional high vacuum volumetric system constructed entirely of Pyrex glass and equipped with grease-free valves. Vacuum was created by a mechanical pump E2M1.5 (Edwards) reaching residual pressures of 10⁻³ torr. Pressure was registered by a digital display pressure transducer TPR 017 (Balzers) for pressures in the interval of 10⁻⁴ to 1 torr, as well as by a pressure transducer CDG Gauge (Varian) Multi Gage digitally displayed for pressures between 1 and 1000 torr. Before measurement, about 500 mg of each sample (fraction 0.38-0.54 mm) was dehydrated *in situ* at 300 °C in an oven under constant evacuation, down to a residual pressure of 10⁻³ torr, and these conditions were maintained for 3 h. Simultaneously, the determination of the weight loss of the adsorbents was evaluated by heating samples up to 300 °C at atmospheric pressure in a conventional oven. After dehydration, the temperature of the samples was reduced until it reached the desired measuring temperature and it was then maintained constant for at least 1 h before starting any measurement. The 0 °C temperature was created by a bath of ice water. The 20 and 60 °C temperatures were controlled by a Haake L. ultra thermostat with a precision of ± 0.15 °C, while the 100 °C temperature was controlled by an oven (Lindberg) with a precision of ± 0.2 °C.

Gas adsorption uptake as a function of time was obtained as the difference between the initial amount of gas introduced into the cell and the amount of gas remaining in the dead space of the cell at any given time between 0 and *t*_{eq} (equilibrium time). The initial pressure was 400 torr in all experiments.

During the kinetic measurements, the pressure decrease in the system was measured manually and this allowed us to write down time and pressure data. The procedure used to perform the kinetic measurements was described in detail in previous papers (Aguilar-Armenta *et al.* 2001, Aguilar-Armenta *et al.* 2006). After evacuation of the adsorbent *in situ* at 300 °C, a kinetic adsorption curve was measured at a given temperature. Subsequently, the sample was evacuated at 300 °C, as in the previous experiment, until a residual pressure of < 10⁻³ torr was reached for another study.

RESULTS AND DISCUSSION

Adsorption kinetics

Adsorbate uptake curves for N₂O were measured from *t* = 0 up until equilibrium was reached (*t* → ∞, *a* = constant).

a) ZAPS. Figure 1 shows the adsorption kinetic curves for N₂O on ZAPS at 0, 20, 60, and 100 °C. It can be seen that the adsorbed amount and the adsorption rate diminish with increasing temperature. This behavior allows us to deduce that the adsorption process of N₂O is not of the activated type and that it is probably not influenced by kinetic effects, possibly because the kinetic diameter of the N₂O molecule is 3.3 Å (Breck 1974) and ZAPS adsorbs molecules with kinetic diameters that do not exceed 4.3 Å.

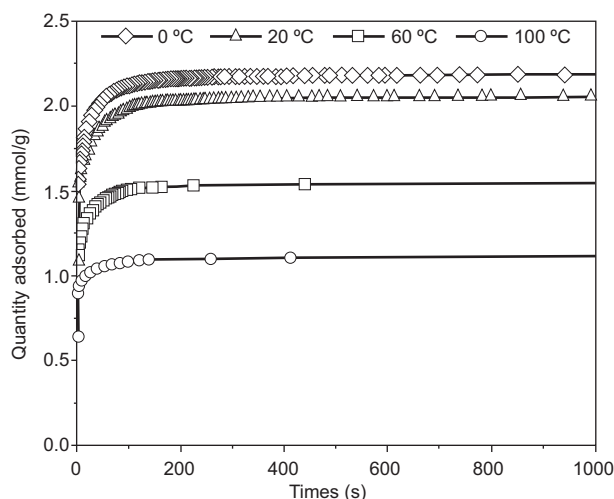


Fig. 1. Uptake rates of N₂O on erionite at different temperatures

To study more carefully the effect of temperature on the adsorption rate of gas, the fractional pore filling a/a_{∞} , where a and a_{∞} are the amounts adsorbed at a given time t and at equilibrium, respectively, was analyzed as a function of time. The adsorption rate of the fractional uptake of N₂O on ZAPS is shown in figure 2. The results show that for times as short as 100 seconds, a 90 % of the total capacity of N₂O adsorption is observed. In addition, the adsorption rate of N₂O does not depend on temperature in the range of 0-100 °C (fig. 2), confirming that this process is not an activated diffusion.

The values of the diffusion coefficients (D , cm²/s) were found by fitting the experimental data by the Barrer equation $R = a_t - a_0/a_{\infty} - a_0 = 2S_{BET}/V(1 + K/K_0)(Dt/\pi)^{1/2}$ (Barrer 1971). Where $K = [(a_0)_g - (a_{\infty} - a_0)/a_{\infty}]$ is the ratio of the adsorbate in the gas phase to that in the adsorbed phase at equilibrium; a_t , a_0 and a_{∞} are the amounts of gas adsorbed at times t , $t = 0$, and $t = \infty$ (equilibrium), respectively (in our experiments $a_0 = 0$); $2S_{BET}$ and V are the specific external surface area of the particles (cm²/g) and the volume of the crystals (cm³/g), respectively; $(a_0)_g$ is the amount of

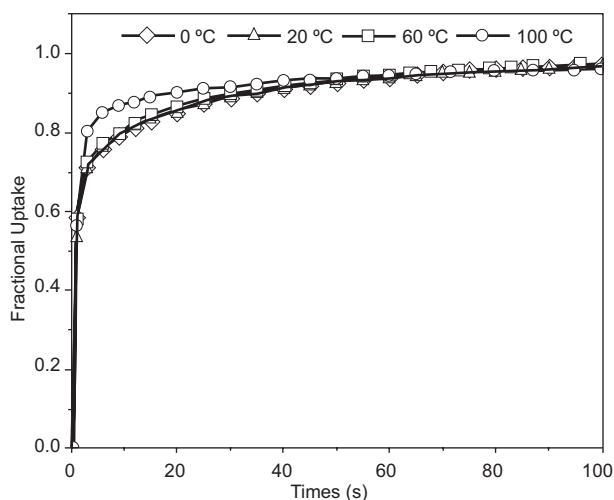


Fig. 2. N₂O fractional uptakes on erionite at different temperatures

gas initially available for adsorption; D is the diffusion coefficient (cm²/s). Table I summarizes the diffusion time constants of N₂O on ZAPS at different temperatures. These results show that the diffusion of N₂O rises faster with increases of temperature between 20 and 100 °C.

The activation energy can be calculated by the equation $Ea = [RT_1T_2/T_1] \ln[\tau_{2(0.5)}/\tau_{2(0.5)}]$ (Timofeev *et al* 1961). Calculations revealed that the energy of activation in ZAPS is 1.8 kJ/mol (Table I).

b) ZSL. The adsorption kinetic behavior at 0, 20, 60, and 100 °C on the ZSL sample for N₂O is presented in figure 3. These results show that the

TABLE I. DIFFUSION COEFFICIENTS (D) AND DIFFUSION ACTIVATION ENERGIES (E_a) OF N₂O ON THE STUDIED ZEOLITES: ERIONITE (ZAPS), MORDENITE (ZNT), AND CLINOPTILOLITE (ZSL)

Adsorbent	Temperature (°C)	$D \times 10^{15}$ (cm ² /s)	E_a (kJ/mol)
ZAPS	0	0.010	1.8
	20	0.005	
	60	0.008	
	100	0.060	
ZNT	0	0.003	4.3
	20	0.012	
	60	0.067	
	100	0.204	
ZSL	0	0.032	4.6
	20	0.012	
	60	0.688	
	100	1.890	

adsorbed amount and the adsorption rate diminish with increasing temperature, as in the case of the ZAPS sample. It can be seen that the adsorbed amounts of N_2O on the ZSL sample is lower than that on the ZAPS sample (**fig. 1**). The latter could be due to the decrease in micropore accessibility (3.5 Å). The fractional uptakes of N_2O on ZSL at different temperatures reveal a great difference in the adsorption kinetic behavior on the ZAPS and ZSL samples (**Fig. 4**). The adsorbed amounts of N_2O on ZAPS, in the range from $t = 0$ to $t = t_{eq}$ (equilibrium) at different temperatures, were greater than that on ZSL. The activation energy on ZSL was 4.6 kJ/mol. These results show that the diffusion of N_2O rises faster on ZSL than that on ZAPS as the temperature increases

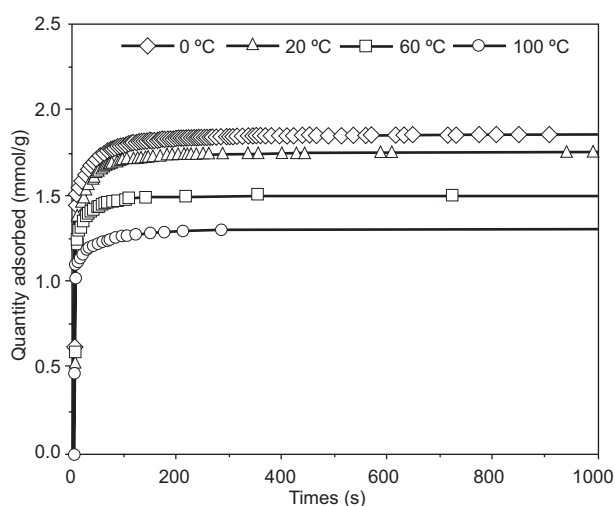


Fig. 3. Uptake rates of N_2O on clinoptilolite at different temperatures

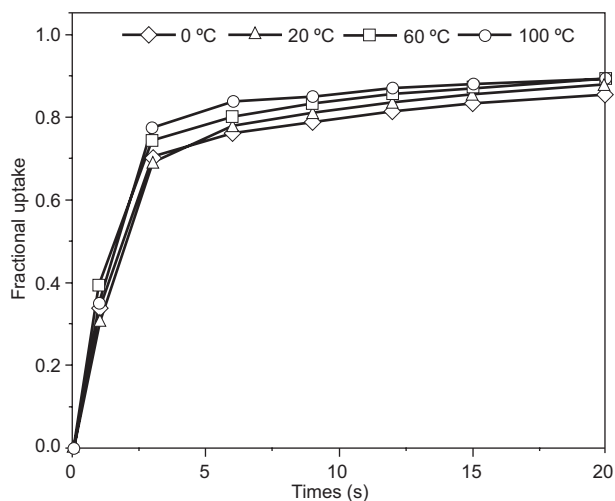


Fig. 4. N_2O fractional uptakes on clinoptilolite at different temperatures

(**Table I**). Taking into account that the kinetic diameter of N_2O is about 3.3 Å, while the ZSL diameter is around 3.5 Å, we believe that these results could be due to the lower micropore participation in the N_2O adsorption process.

c) ZNT. The results shown in **figures 5 and 6** reveal a decrease in adsorption uptake when the temperature goes up from 0 to 100 °C in ZNT. These results show that the adsorption process of N_2O is not of the activated type and that it is probably not influenced by kinetic effects. Unlike for ZAPS and ZSL, the activation energy was 4.3 kJ/mol. This could be due to the reduction of pore volume that

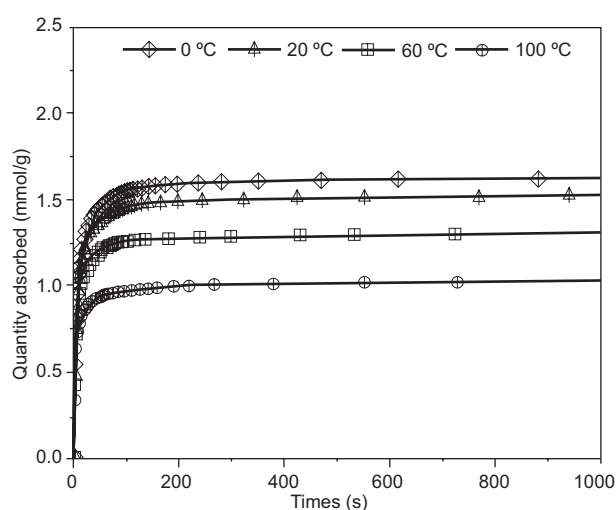


Fig. 5. Uptake rates of N_2O on mordenite at different temperatures

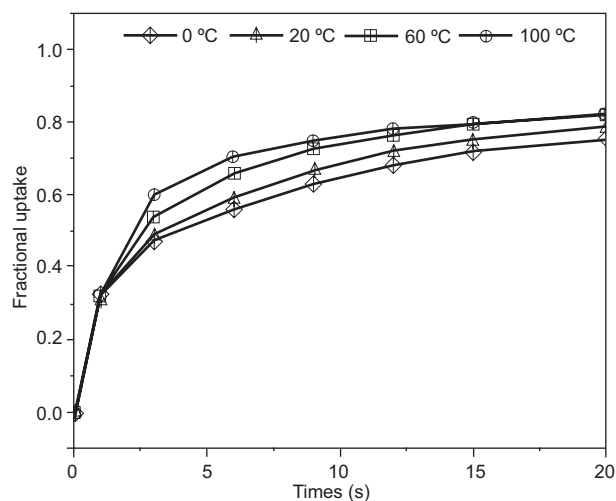


Fig. 6. N_2O fractional uptakes on mordenite at different temperatures

greatly influences the adsorption of the N₂O molecule (Hernández-Huesca *et al.* 1999). The diffusion constants of N₂O are of a higher order as temperature increases, these values are also higher to one another (Table I).

Influence of the temperature in the adsorption of N₂O

The N₂O adsorption capacities decrease in the order ZAPS > ZSL > ZNT at 20 °C (Figs. 1, 3 and 5). Therefore, this adsorption behavior is mainly due to the limiting volume of the micropores of these zeolites and to the quantity of cations available per unit mass of the dehydrated zeolites (cationic density). The cationic density depends on the Si/Al ratio, which follows precisely the order ZSL ≈ ZNT > ZAPS (Hernández-Huesca *et al.* 2009). In other words, the adsorption capacity of ZAPS is the greatest because there is a larger amount of Al in this zeolite and, therefore, its cationic density is greater than that of the other two zeolites.

There is a difference between the adsorbed amounts of N₂O at 20 °C than at 100 °C. The results show that the adsorption capacities decrease in the order ZSL > ZAPS > ZNT at 100 °C. This behavior suggests that the adsorption of N₂O is favored at low temperatures on ZAPS, close to room temperature, whereas the adsorption of N₂O is recommended at 100 °C on ZSL.

CONCLUSIONS

Within the temperature range studied, the adsorbed amount and the adsorption rate of N₂O diminish with increasing temperature in zeolites. This behavior allows us to deduce that the adsorption process of N₂O is not of the activated type and that it is not influenced by kinetic effects. The capacities of these samples to adsorb N₂O increase in the order ZNT < ZSL < ZAPS due to higher cationic density (Si/Al) and their corresponding properties. It was established that the adsorption of N₂O on ZAPS can be effected most efficiently at ambient temperature (20 °C), whereas the use of ZSL could be recommended at 100 °C. The activation energies (kJ/mol) for the adsorption of N₂O were 1.8, 4.3 and 4.6 on ZAPS, ZNT and ZSL, respectively.

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